

Supporting information for:

**Modelling and simulation of CLC using a
copper-based oxygen carrier in a double loop
circulating fluidized bed reactor system**

Yuanwei Zhang,^{*,†} Øyvind Langørgen,[‡] Inge Saanum,[‡] Zhongxi Chao,[¶] and
Hugo A. Jakobsen[†]

[†]*Department of Chemical engineering, Norwegian University of Science and Technology,
Sem Sælandsvei 4, 7034 Trondheim, Norway*

[‡]*SINTEF Energy Research, Sem Sælands vei 11, 7034 Trondheim, Norway*

[¶]*Safetec Nordic AS, Klæbuveien 194, 7037 Trondheim, Norway*

E-mail: yuanwei.zhang@ntnu.no

Table S1: Closure for turbulent model

Turbulent viscosity
$\mu_g^t = \rho_g C_\mu \frac{k_g^2}{\varepsilon_g}$
Turbulent kinetic energy production [?]
$S_t = C_b \beta (\vec{v}_s - \vec{v}_g)^2$
Turbulent stress tensor [?]
$\bar{\tau}_t = -\frac{2}{3} \rho_g k_g \bar{\mathbf{I}} + 2\mu_g^t \bar{\mathbf{S}}_g$

Table S2: Empirical parameters for the $\kappa - \varepsilon$ model.

C_μ	σ_0	σ_ε	C_1	C_2	C_b
0.09	1.00	1.30	1.44	1.92	0.25

Table S3: Constitutive equations for internal momentum transfer

Gas phase stress
$\bar{\tau}_g = 2\alpha_g\mu_g\bar{\bar{S}}_g$
Solid phase stress
$\bar{\tau}_s = -(-p_s + \alpha_s\mu_{B,s}\nabla \cdot \vec{v}_s) - 2\alpha_s\mu_s\bar{\bar{S}}_s$
Deformation rate for phase k ($k = g, s$)
$\bar{\bar{S}}_k = \frac{1}{2}(\nabla \vec{v}_k + (\nabla \vec{v}_k)^T) - \frac{1}{3}(\nabla \cdot \vec{v}_k)\bar{\mathbf{I}}$
Solid phase pressure?
$p_s = \alpha_s\rho_s\Theta_s[1 + 2(1 - e)\alpha_sg_0]$
solid bulk viscosity?
$\mu_{B,s} = \frac{4}{3}\alpha_s\rho_sd_pg_0(1 + e)\sqrt{\frac{\Theta_s}{\pi}} + \frac{4}{5}\alpha_s\rho_sd_pg_0(1 + e)$
Solid phase shear viscosity?
$\mu_s = \frac{2\mu_s^{dilute}}{\alpha_sg_0(1 + e)}\left[1 + \frac{4}{5}\alpha_sg_0(1 + e)\right]^2 + \frac{4}{5}\alpha_s\rho_sg_0(1 + e)\sqrt{\frac{\Theta_s}{\pi}}$
Conductivity of the granular temperature?
$\kappa_s = \frac{15}{2}\frac{\mu_s^{dilute}}{(1 + e)g_0}\left[1 + \frac{6}{5}\alpha_sg_0(1 + e)\right]^2 + 2\alpha_s^2\rho_sd_p(1 + e)g_0\sqrt{\frac{\Theta_s}{\pi}}$
Collisional energy dissipation?
$\gamma_s = 3(1 - e^2)\alpha_s^2\rho_sg_0\Theta_s\left[\frac{4}{d_p}\sqrt{\frac{\Theta_s}{\pi}} - \nabla \cdot \vec{v}_s\right]$
Radial distribution function?
$g_0 = \frac{1 + 2.5\alpha_s + 4.5904\alpha_s^2 + 4.515439\alpha_s^3}{\left[1 - \left(\frac{\alpha_s}{\alpha_s^{max}}\right)^3\right]^{0.67802}}$
Dilute viscosity?
$\mu_s^{dilute} = \frac{5}{96}\rho_sd_p\sqrt{\pi\Theta_s}$
Interfacial force
$\vec{M}_g = -\vec{M}_s = \beta(\vec{u}_s - \vec{u}_g)$
Drag coefficients?
$\beta = C\left[\frac{17.3}{Re_p} + 0.336\right]\frac{\rho_g}{d_s} \mathbf{v}_s - \mathbf{v}_g \alpha_s\alpha_g^{-1.8}$

Table S4: Constitutive equations for mass transfer

Effective diffusivity
$D_{k,j}^e = D_{k,j}^m + D_k^t$
Molecular diffusion coefficient [?]
$D_{g,j}^m = \frac{1 - \omega_j}{M_m \sum_{j \neq i} \frac{\omega_j}{M_j D_{ji}}}$
Binary diffusion coefficient [?]
$D_{ji} = \frac{T_0^{1.75} \sqrt{1/M_j + 1/M_i}}{101.325 P \left((\sum V)_j^{1/3} + (\sum V)_i^{1/3} \right)^2}$
Turbulent diffusion coefficient [?]
$D_g^t = \frac{\mu_g^t}{\rho_g Sc^t}$
$D_s^t = \frac{d_p}{16\alpha_s} \sqrt{\pi} \Theta$

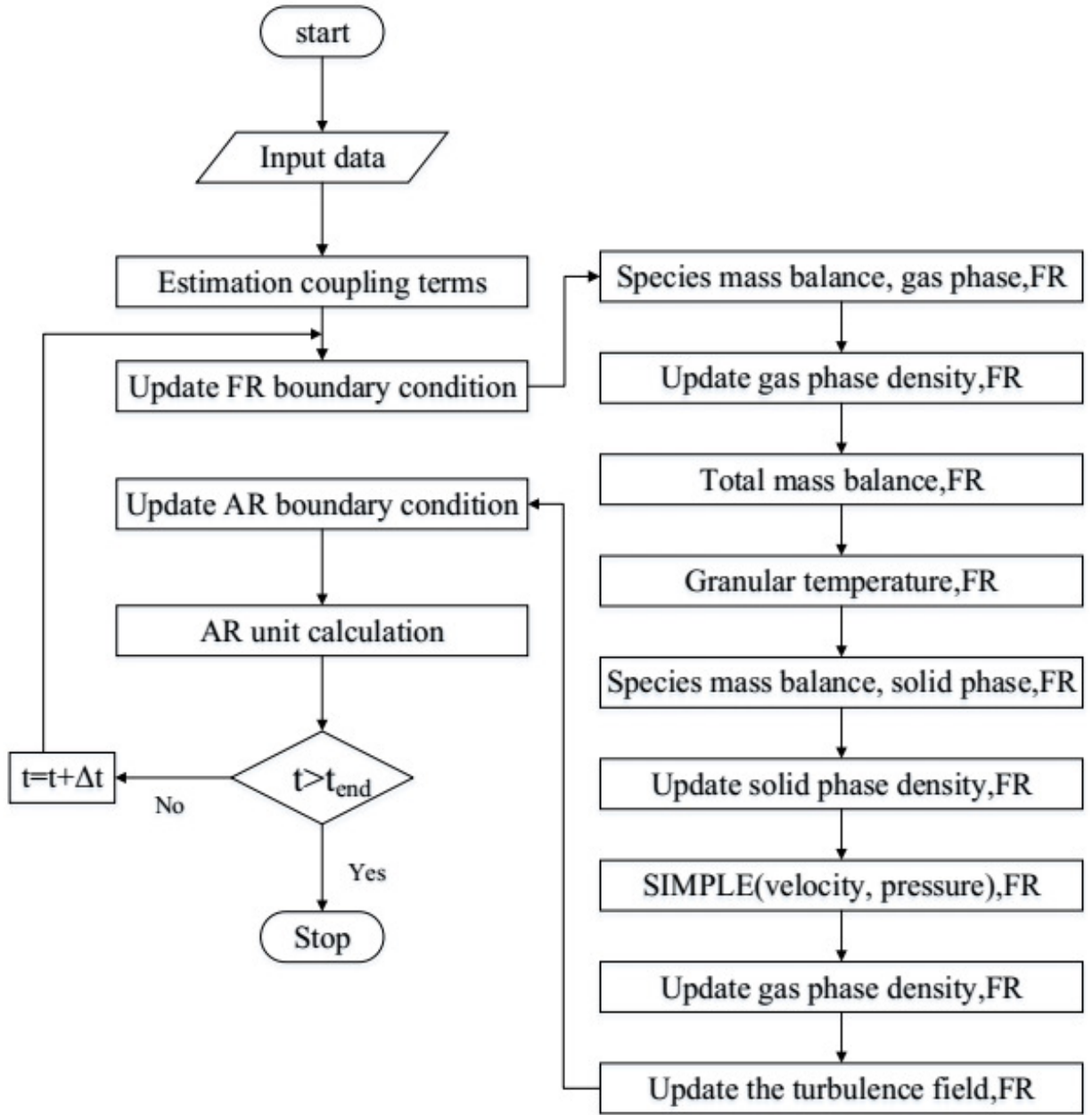


Figure S1: Sketch of the numerical solution algorithm