

1
2
3
4
5
6
7
8
9
10
11
12
13
14
15
16
17
18
19
20
21

Supporting Information

The influence of electric fields on biofouling of carbonaceous electrodes

Soumya Pandit¹, Sneha Shanbhag², Meagan Mauter^{2,3}, Yoram Oren¹ and Moshe Herzberg^{1*}

Author Affiliations:

¹ Zuckerberg Institute for Water Research, Blaustein Institutes for Desert Research, Ben Gurion University of the Negev, Midreshet Ben Gurion, 84990, ISRAEL

² Department of Civil & Environmental Engineering, Carnegie Mellon University, 5000 Forbes Ave., Pittsburgh, PA, 15213, USA

³ Department of Engineering and Public Policy, Carnegie Mellon University, 5000 Forbes Ave., Pittsburgh, PA, 15213, USA

*Author to Whom Correspondence Should Be Addressed

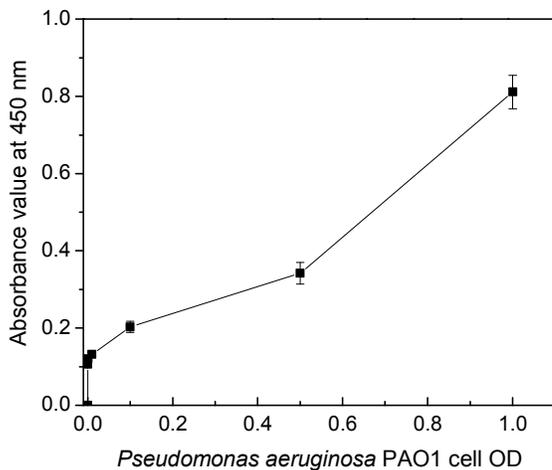
E-mail: herzberg@bgu.ac.il

Phone: +972-86563520

Number of pages: S1-S23 (23)

Number of figures: S1-S16 (16)

22 **SI-1 Growth curve experiment for wild type *Pseudomonas aeruginosa* PAO1 and**
23 **Calibration curve of XTT assay**



24

25 **Figure S-1: Calibration curve of XTT assay**

26

27 **SI-2 Construction of the customized flow cell**

28 A customized parallel plate electrochemical flow-cell was constructed and the details
29 of preparation steps are explained as follows: (1) The reference electrode terminal was
30 attached to the counter electrode terminal by a crocodile clip; (2) the working electrode
31 terminal was connected to a thin aluminum foil (1.5 μm) via a copper stick; (3) an indium
32 tin oxide (ITO)-covered electrically conductive glass slide was wired to a potentiostat
33 instead of a regular cover-glass using a platinum foil; and (4) the carbon or graphite at the
34 bottom of the flow chamber was used as working electrode. The constant voltage was
35 applied with a potentiostat (Princeton Applied Research), and then the resulting electric
36 current was monitored via the affiliated computer program (ECHEM). The voltage was
37 also recorded by a data-logger (EXTech Instruments). Additionally, the working
38 electrode for biofilm growth study was connected with a thin aluminum foil as a current
39 collector. The conductive side of ITO slide was adjusted to a 0.5 μm thick platinum frame
40 at its edges in order to distribute the electrical potential as much uniformly as possible
41 throughout the entire flow-channel.

42

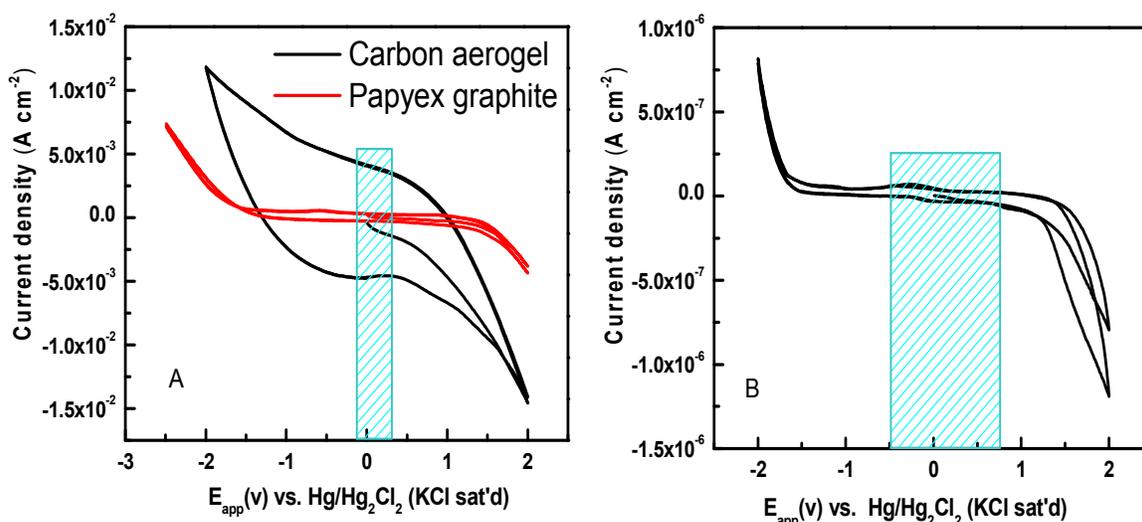
43 **SI-3 Determination of working and counter electrode's voltage window**

44 The range of voltages applied to the electrodes (voltage window) is an important
45 parameter in the flow cell experiments. In general, a potential range should be selected
46 where current does not change abruptly with applied potential. In this research, the
47 effective voltage window of the different working and counter electrodes were studied by
48 cyclic voltammetry (CV) using Princeton 273a potentiostat. A three-electrode
49 configuration consisting of PA, CA and ITO coated glass as working electrodes and Pt
50 wire and Hg/Hg₂Cl₂ (KCl sat'd) as counter and reference electrodes, respectively, was
51 used for all the CV measurements using an electrochemical cell (Metrohm Autolab). The
52 solution was the same as used in the flow cell experiments, namely, 10% LB medium
53 supplemented with 0.1 M Na₂SO₄. Cyclic voltammograms (Figures S-2 A and B) were
54 recorded in the potential range of -2.0 V to +2.0 V at a scan rate of 5 mV/s. The initial
55 and final potential was kept constant at 0.1 V (close to OCP).

56 In the flow cell experiments, different voltages were applied between the counter (ITO)
57 electrode and the working (PA or CA) electrodes at the voltage range +0.9V to -0.9 V.
58 This corresponds to a voltage window of -70mV to +250mV while at the same time that
59 for ITO was between -550mV and +350 mV (all values are vs. Hg/Hg₂Cl₂, KCl sat'd).
60 As depicted in Figures S-2A and S2-B by the dashed bars, these windows are well within
61 the range where Faradic reactions (such as water electrolysis) can be considered
62 insignificant. These ranges correspond to a maximum voltage window of -0.9V to +0.9V
63 between the working (PA or CA) and the counter (ITO) electrodes. As depicted in Figure
64 S-2A by the dashed bar, this window is well within the range were Faradic reactions
65 (such as water electrolysis) can be considered insignificant.

66

67



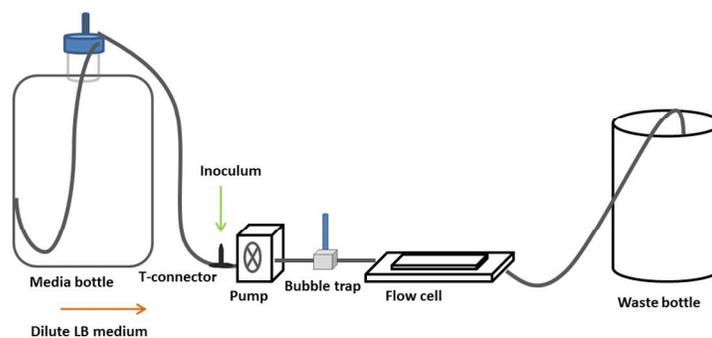
68 **Figure S-2:** Cyclic voltammograms at a scan rate of 5 mV/sec using 10% LB medium
 69 supplemented with 0.1 M Na₂SO₄ as an electrolyte. A) Working electrodes- Carbon
 70 aerogel and Papyex graphite. B) ITO coated glass slide. The dashed bar in Figure A
 71 shows the voltage range, in terms of working electrode vs. reference electrode,
 72 corresponding to the voltage range applied in the flow cell experiments.

73

74

75 **SI-4 Scheme of flow cell set-up**

76



77

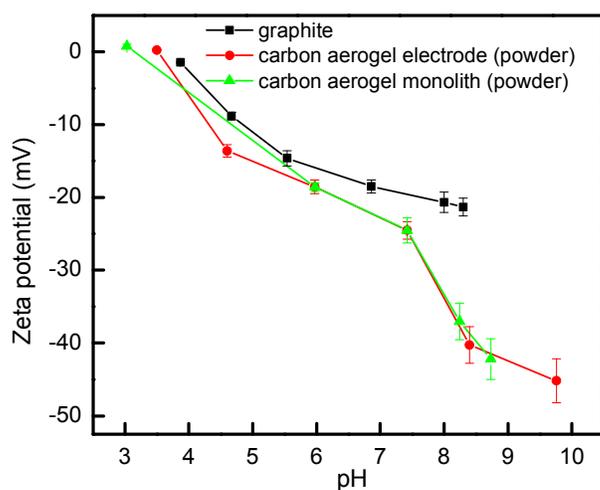
78

Figure S-3: Schematic of flow cell set-up

79 **SI-5 Zeta potential measurements for carbon electrodes**

80 As it is shown in Figure S-4, there was not any significant difference between the zeta
81 potentials of monoliths versus electrodes. Accordingly, the results demonstrated that at
82 pH above 7, zeta potentials of graphite and carbon aerogel variants diverge, which could
83 be attributed to the pKa values of different chemical functional groups, such as
84 carboxylic and carbonyl group on two different surfaces.

85



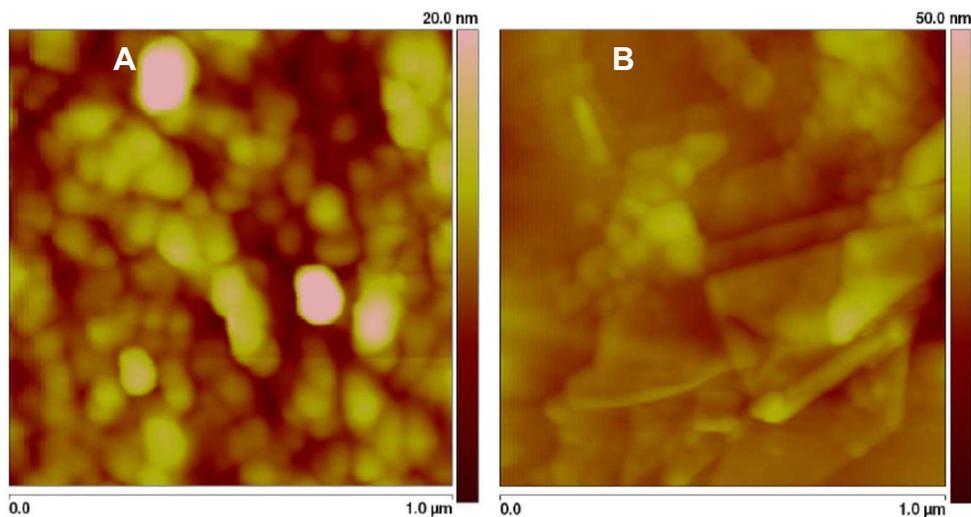
86

87 **Figure S-4.** Zeta potentials of carbon aerogel and graphite vs. pH titrations. All samples
88 were measured in an electrolyte of 0.001 M NaCl and titrated with 0.1M HCl or 0.1 M
89 NaOH. The error bars represent one standard error of at least eight readings

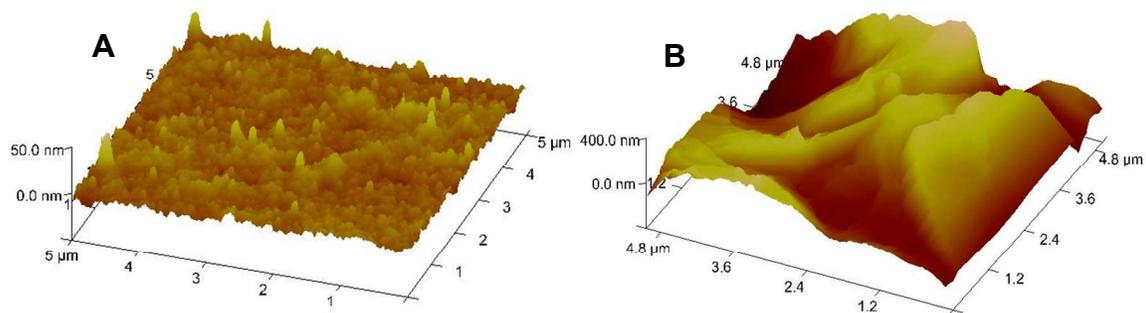
90

91

92 **SI-6 Roughness and topography of the carbon surfaces**



93
94 **Figure S-5:** AFM visualization of carbon aerogel, CA (A) and graphite paper, PA (B) at
95 a resolution of $1 \mu\text{m}^2$. The z-scale is depicted on the right to each frame and covers a
96 broader range in graphite.



97 **Figure S- 6:** 3D visualization of carbon aerogel, CA- A; and graphite, PA- B: at a
98 resolution of $5 \mu\text{m}^2$. In graphite, the range of the z-scale is four times the range in carbon
99 aerogel.

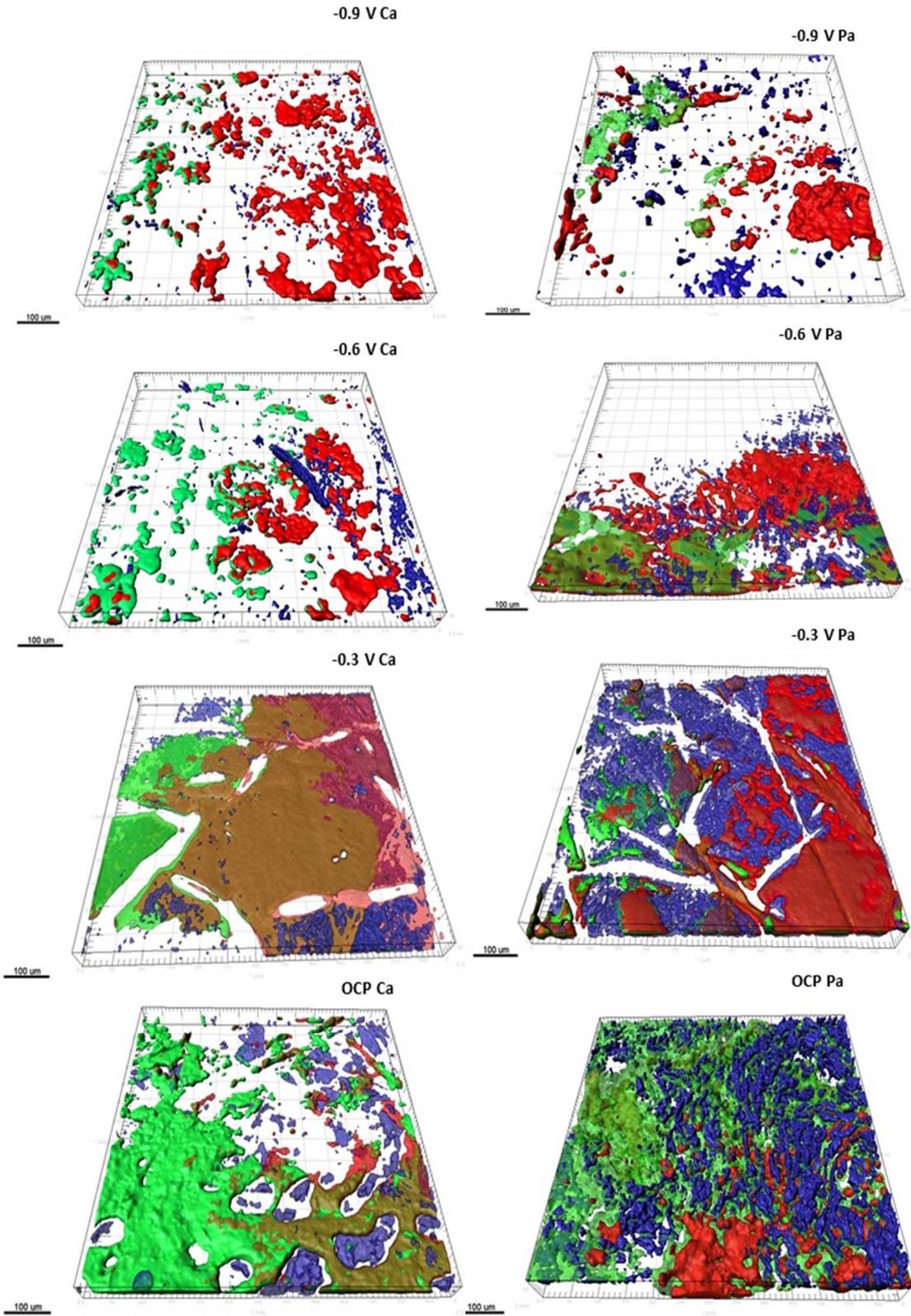
100

101 **SI-7 Investigating the interaction between the produced formazan salt dye with**
102 **carbon particles**

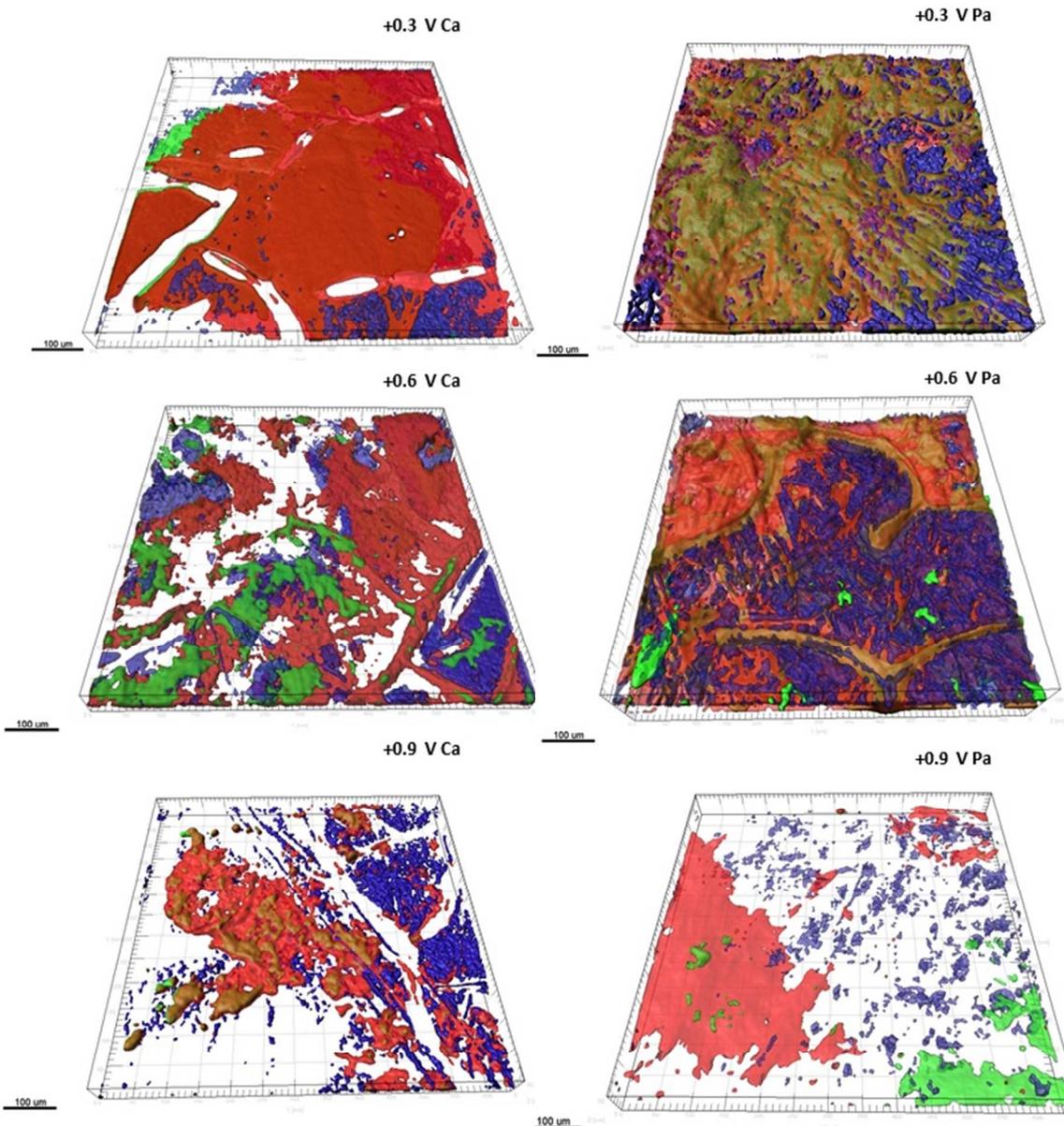
103 In order to prove the lack of any interaction between the produced formazan salt dye with
104 carbon particles, formazan salt containing solution was collected after 2 h incubation in a
105 multiplate reader instrument with XTT reagent and bacterial suspension. After
106 centrifugation, the supernatant was divided in to halves of 50 μ L and 50 μ L. Then DDW
107 was added in one Eppendorf tube while 50 μ L carbon particles suspended solution was
108 added to the other one. It is worth mentioning that the experiment was done in dark room
109 to avoid photo bleaching. The absorbance measurements were carried out after keeping
110 both Eppendorf micro-centrifuge tubes stationary for two hours. The results did not show
111 any of significant difference in absorbance intensity (≈ 0.6). Hence, this experiment
112 indicated no interaction of produced formazan salt dye with carbon particles.

113

114 SI-8 IMARIS 3-D reconstruction images from CLSM analysis for qualitative
115 analysis of the biofilm morphology.



116



117

118 *Figure S-7: IMARIS 3-D images: The left and right columns present the exemplary*
 119 *images from scans of carbon aerogel (Ca) and Papyex graphite (Pa), respectively.*
 120 *The red, green, and blue clusters indicate dead cells, live cells, and EPS on electrode,*
 121 *respectively. The orange and violet colour indicate overlapping zones of live and*
 122 *dead cells, as well as dead cells and EPS, respectively. Figures are perspective*
 123 *images 600 μm × 600 μm in size.*

124

125

126 **SI-9 Effect of an electric field on the thickness of biofilm on carbon electrodes**

127

128

129

130

131

132

133

134

135

136

137

138

139

140

141

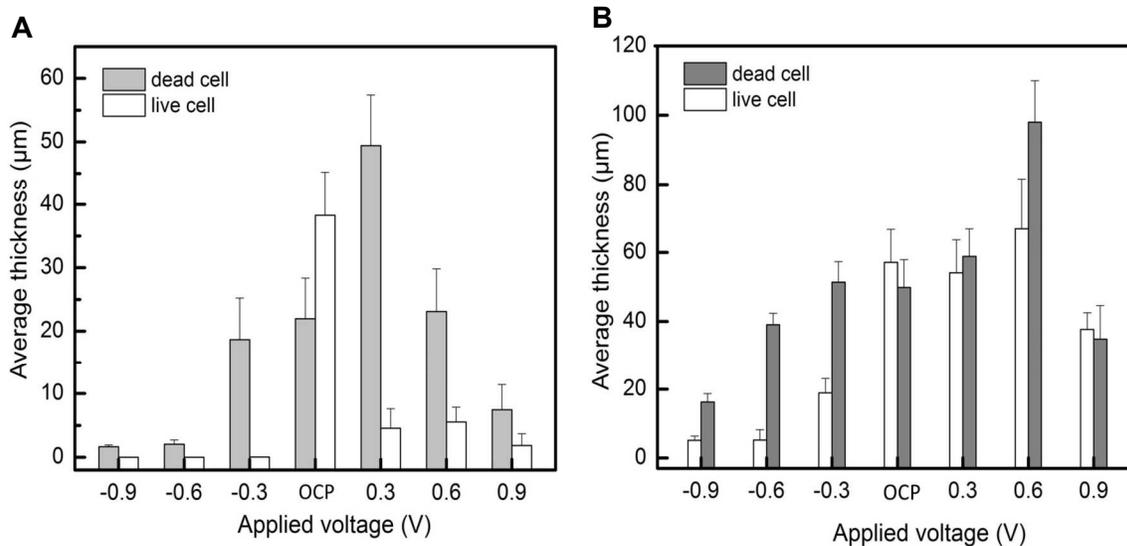


Figure S-8: The average thickness value at A: CA and B: PA in flow cell experiment using 10% LB (Luria-Bertani) medium after 36 hours. Each error bar represents one standard error.

142 **SI-10 Effect of an electric field on EPS formation on a carbon electrode**

143

144

145

146

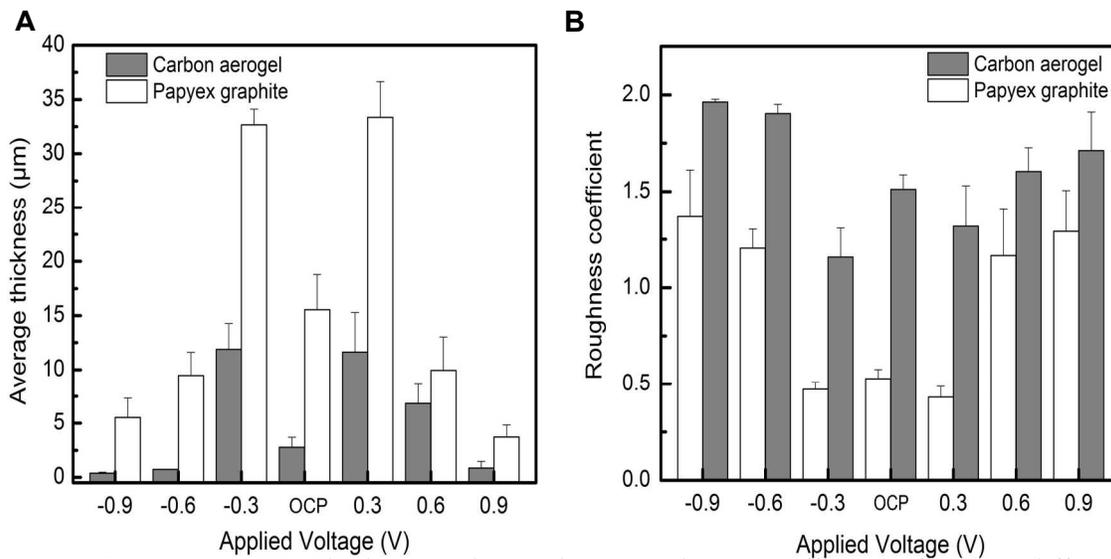
147

148

149

150

151

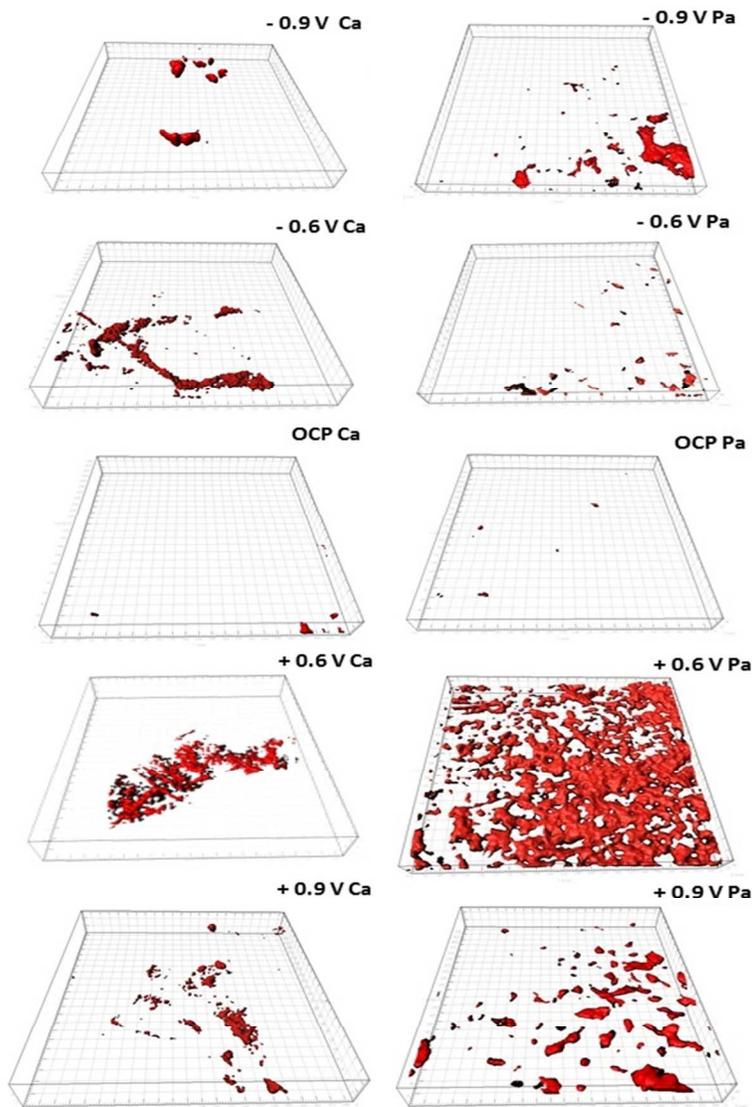


152 **Figure S-9:** A: Average thickness value and B: Roughness coefficient of EPS at different
153 carbon electrode in flow cell experiment using 10% LB (Luria-Bertani) medium; each
154 error bar represents one standard error. 0 V implied open circuit condition (without any
155 external applied potential).

156

157

158 SI-11 Analysis of intracellular ROS using DHR assay and observed in IMARIS
159 visualizations of the CLSM results



160

161 **Figure S-10:** IMARIS 3-D images: Analysis of intracellular ROS using DHR assay. The
162 left and right columns present the exemplary images from scans of carbon aerogel (CA)
163 and Papyex graphite (PA), respectively, polarized at different magnitude of applied
164 potential. The red cluster indicated DHR stained bacterial cell on electrode. Figures are
165 perspective images $600 \mu\text{m} \times 600 \mu\text{m}$ in size.

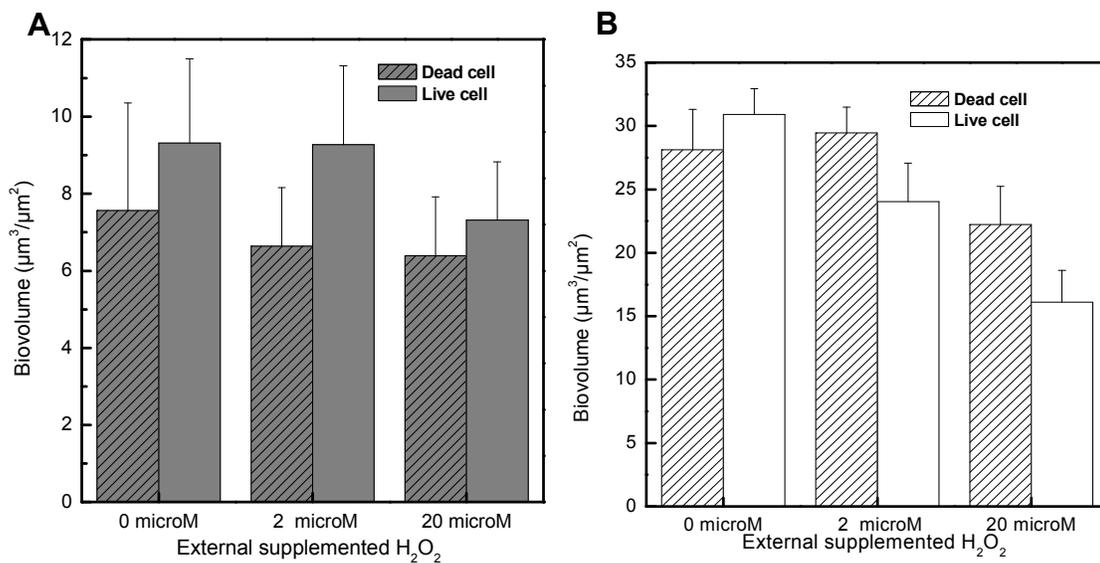
166

167

168 **SI-12 Effect of external dosage of hydrogen peroxide on biofilm formation at OCP**
169 **condition**

170 In order to provide a quantitative measure for the effect of peroxide on biofilm
171 formation in this study, additional experiments were carried out to confirm the influence
172 of external dosage of HP on biofilm formation at open circuit mode as it is described in
173 this section.

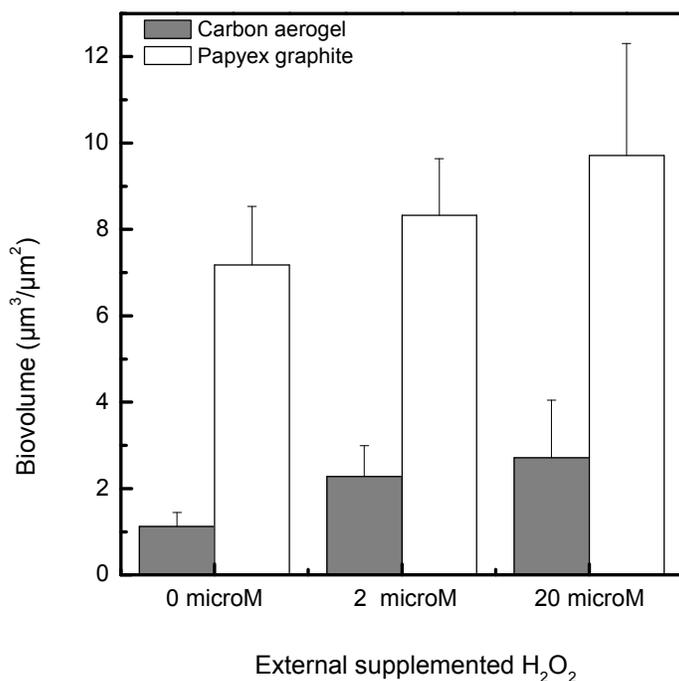
174 Two different concentrations were supplemented to the flow cell during generation of
175 biofilm on the carbon electrode: 2 μ M and 20 μ M HP (a 10 fold higher in order to
176 evaluate the effect of external HP dosing) at open circuit mode. The effect of external HP
177 dosing at open circuit mode was carried out by providing diluted HP from external source.
178 The generated biomass was now compared with biomass generated without H₂O₂ dosing
179 at OCP. The biovolume generated without HP and with 2 μ M was almost similar while
180 using 20 μ M HP (Figure S-11 A & B), the biovolume for both dead and live cell was
181 slightly lower. This might be due to damage of seed bacteria adsorb on the electrode
182 surface. Similar trend was noticed for both Papyex graphite and carbon aerogel. EPS
183 production increased with increasing dosing of HP suggesting retaliation of biofilm to
184 negate the harmful effect of HP (Figure S-12). This part of the study indicated
185 insignificant effect of HP on biofilm formation when its concentration is lower, which
186 may relate to diffusion limitation in the flow cell. While this experiment was carried out
187 intending to simulate the situation on the electrode under the influence of external electric
188 field, this situation is different from the HP generation on the polarized electrode. At
189 cathodically polarized condition, HP instantly generated on the surface of electrode (E_{app}
190 > 0.5 V) and it may cause impairment of bacterial cell adsorbed on the surface of the
191 working electrode due to the intimate proximity of the bacterial cell and the source of HP.



192

193 **Figure S-11:** Biovolumes of dead cell and live cell generated on different carbon
 194 electrodes after 36 hour of flow cell experiment using 10% LB (Luria-Bertani) medium.
 195 A: CA and B: PA; Each error bar represents one standard error. The X axis represents
 196 different concentration of H₂O₂ supplemented in flow cell.

197



198

199 **Figure S-12:** Biovolumes of EPS generated on different carbon electrodes after 36 hour
 200 of flow cell experiment using 10% LB (Luria-Bertani) medium. Each error bar represents
 201 one standard error. The X axis represents different concentration of H₂O₂ supplemented
 202 in flow cell.

203

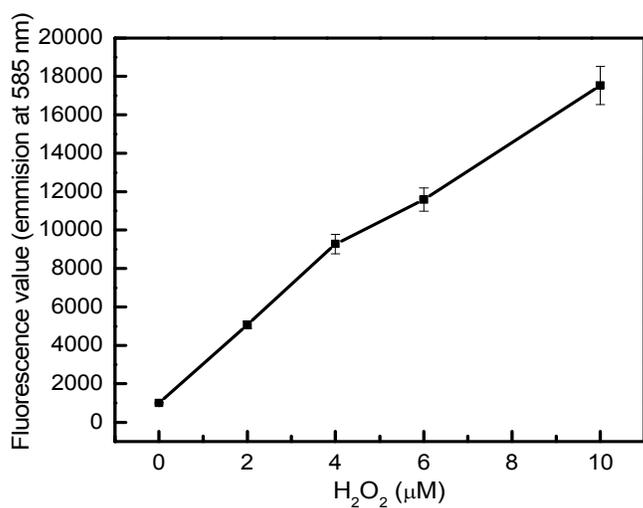
204 **SI-13 Effect of electric field on production of hydrogen peroxide**

205 In order to confirm the generation of HP, under the studied conditions, the Amplex red
 206 HP assay was used. A Standard curve for HP quantification using Amplex red® HP assay
 207 was provided in S-13. It should be mentioned that the online measurement of HP
 208 generation in a continuous flow cell containing bacteria is challenging, because solution
 209 collected from the outlet for HP measurement needed filtration to separate detached cells
 210 or unwanted clump. In order to resolve these challenges and collecting more accurate
 211 data of the electrochemical HP generation, electrodes were polarized without bacterial
 212 inoculation while flow cell was kept in batch mode. The batch mode was opted to avoid
 213 the possible ‘washout’ of HP in continuous mode flow cell experiment. This method’s

214 implementation could avoid the complication associated with biological matter during the
215 HP measurements.

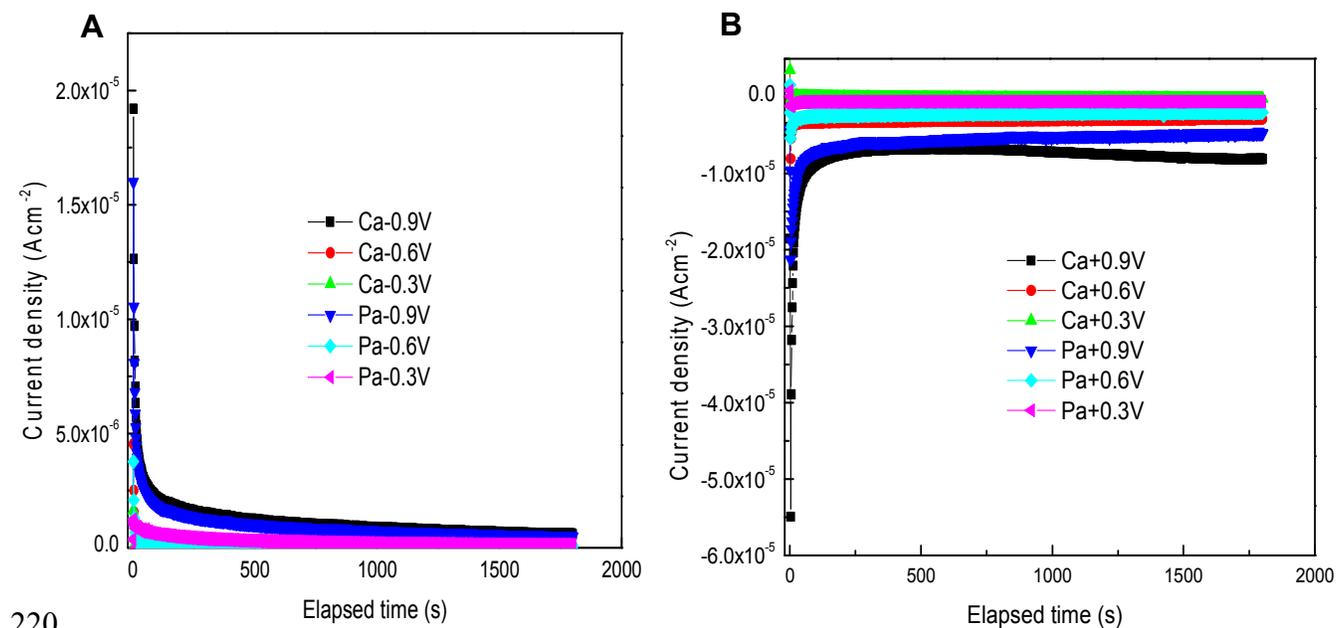
216

217



218

219 **Figure S-13** Standard curve for HP quantification using Amplex red® HP assay



220

221 **Figure S-14:** Chronoamperometric profile of both carbon aerogel and Papyex at
222 cathodically (A) and anodically (B) polarized condition at the flow cell.

223

224 The current density recorded during chronoamperometry can be correlated to H₂O₂
225 production at different applied voltages. The current density in the very low range of
226 0.002-0.0001 mA/cm² suggested inadequate H₂O₂ generation under the influence of
227 different magnitude of applied potential (Figure S-14).

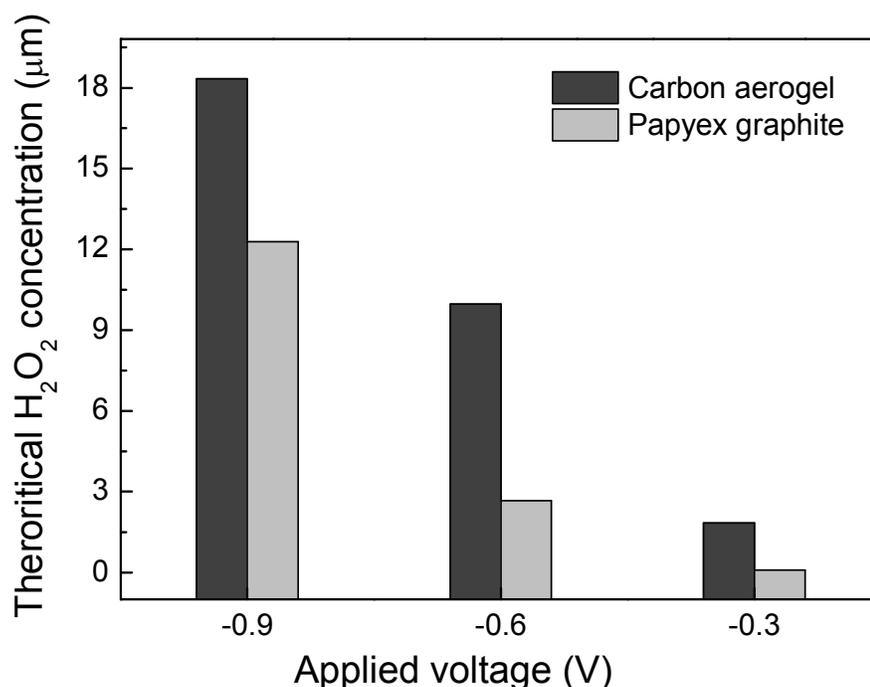
228 **Theoretical generation of hydrogen peroxide along the electrode surface.**

229 We estimated the maximum amount of electrochemically generated HP, along the
230 electrode surface based on the current generated at different magnitudes of applied
231 voltage. The maximum theoretical HP concentration was calculated using equation SI-1
232 assuming 100% Faradic current efficiency (CE) utilized for HP generation and constant
233 current during chronoamperometry.

$$234 \quad C_{H_2O_2} = \frac{CE \int idt}{nFV100} \quad \text{Eq. SI-1}$$

235 where C_{H₂O₂} represents H₂O₂ concentration along the electrode surface (in M) and V is the
236 volume of the electrolyte solution inside the flow cell (in L). n is the number of electrons
237 involved in oxygen reduction reaction to H₂O₂ (2) and F is Faraday constant (96500 C
238 mol⁻¹ e-) (Peralta et al., 2013). Current efficiency (CE) can be defined as the ratio of the
239 electricity consumed by the electrode reaction of interest over the total electricity passed
240 through the circuit (Qiang et al., 2002). The current density values were deduced from the
241 previous experiment of the batch mode HP generation (Figure S-14). Considering 100%
242 faradic efficiency (i.e., all the electrons are assumed to be utilized for H₂O₂ production),

243 the current density and H_2O_2 production on the two different carbon electrodes iare
244 provided in Figure S-15.



245

246 *Figure S-15: The theoretical concentration of H_2O_2 (μM) generated on CA and PA*
247 *carbon electrodes*

248 Assuming 100% Faradic current efficiency, maximum values of 18 and 12 μM HP could
249 be generated along the carbon aerogel and Papyex graphite electrodes, respectively
250 (Figure S-15), while using Amplex red HP assay, a maximum of 2.4 μM of HP was
251 detected. The possible reason for obtaining lower HP concentration during Amplex red
252 HP assay may be due to following reasons: i) instant decomposition of HP; ii) the span
253 of the electrochemically generated HP is short due to instantaneous oxidation of the LB
254 medium.

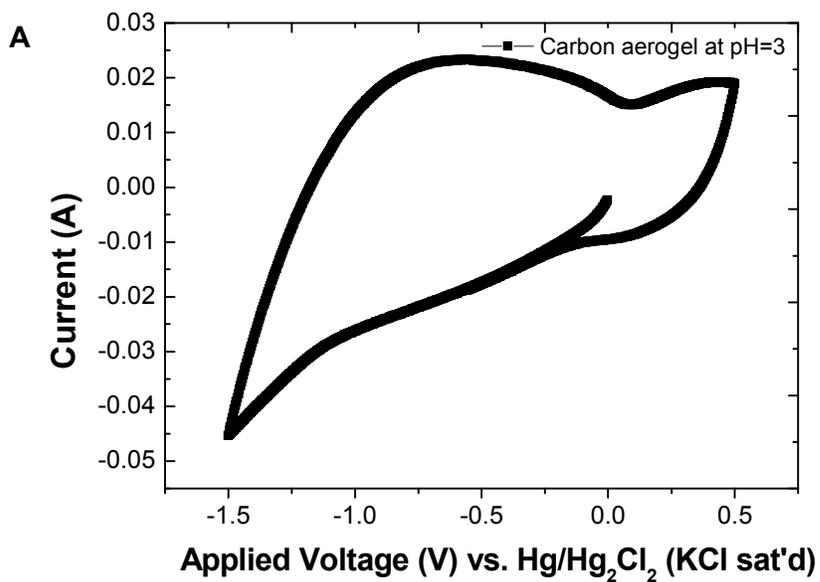
255 In addition, lower concentration of HP may evolve due to physicochemical factors that
256 affect electro- reduction of oxygen. Among them are pH of electrolyte solution, dissolved
257 oxygen concentration and catalytic property of electrode (Sánchez-Sánchez and Bard,
258 2009; Ramaswamy and Mukerjee, 2012).



260 It was reported that

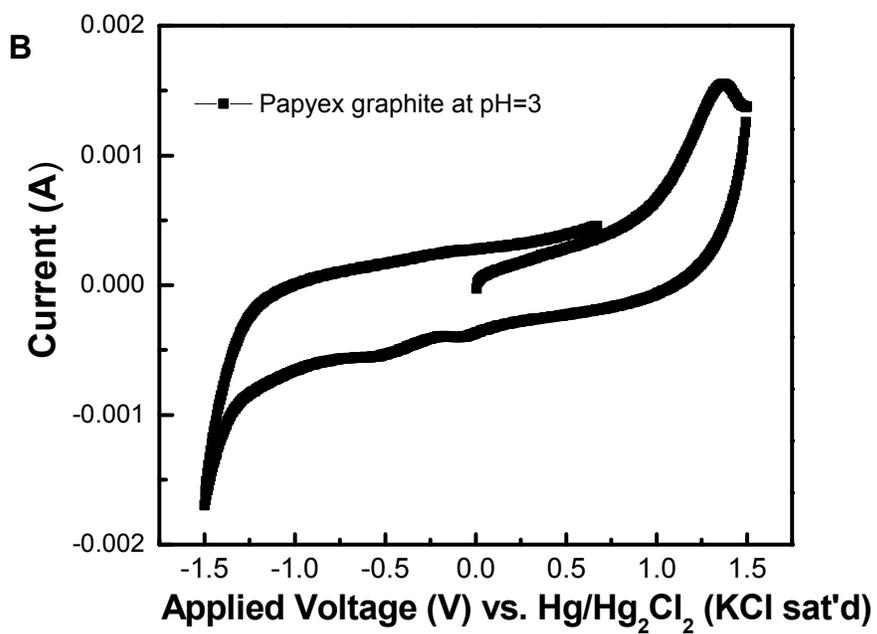
261 pH 3 was reported as optimal for the production of hydrogen peroxide (Peralta et al.,
262 2013)). According to Equation SI-2 indicates that high proton concentration favour the
263 production and accumulation of HP. The nearly neutral pH of the LB media in this study
264 was unfavorable for significant amount of HP production.

265 Figure S-16 shows that the electro-catalytic activity of the carbon aerogel and graphite
266 electrodes is poor at neutral pH. No reduction peak for hydrogen peroxide was detected
267 after adjusting the solution to pH 3 (Figure S-16). Probably, this is the reason why
268 researchers used noble metals (according to volcano plot or surface-modified carbon
269 electrodes for electro-reduction of oxygen for efficient HP production (Jiao et al., 2015).
270 Peralta et al. found a distinct peak at -1.0V (vs. Ag/AgCl) for H_2O_2 from O_2 electro-
271 reduction using cyclic voltammetry (Peralta et al., 2013). Whereas, in this study, we
272 didn't observe similar phenomenon.



273

274



275

276 *Figure S-16: Cyclic voltammograms at a scan rate of 5 mV/sec using 0.1 M 0.1 M*
277 *Na₂SO₄ as an electrolyte at pH 3. A) Working electrodes- Carbon aerogel and B)*
278 *Papyex graphite.*

279 The maximum windows potential range (with respect to saturated calomel electrode) of
280 the present experiment was also not thermodynamically conducive for HP generation
281 (Figure S-2). The maximum cathodic potential with respect to saturated calomel electrode
282 was found around -0.1 to -0.15 mV (Figure S-2). Under this conditions only limited
283 amount of HP generation is expected. Therefore, it can be inferred that all the
284 physicochemical conditions are adverse to HP generation.

285 There are additional reasons, which support the notion that HP effect on the viability of
286 the cells in this study, even at the high calculated magnitude (Figure S-15), is negligible:
287 (i) Catalase (KatA) activity was detected at 50 mM of HP and protected the biofilm cells
288 (Elkins et al., 1999; Stewart et al., 2000) and (ii) relatively high concentration of 44 mM
289 was required to decrease PAO1 biofilm formation (Plyuta et al., 2013).

290 Hence, we conclude that HP generation during the cathodic reduction is sub-inhibitory
291 for biofilm formation. It is noteworthy that bacterial cell viability also reduced when
292 working electrodes were anodically polarized and an elevated intracellular ROS was
293 detected with increase in the magnitude of applied potential. Therefore, the intracellular
294 ROS generation towing to the applied electrode potential is the main cause for the non-
295 viability of the bacterial biofilm cells.

296

297

298 **References**

- 299 Elkins, J.G., Hassett, D.J., Stewart, P.S., Schweizer, H.P., McDermott, T.R., 1999.
300 Protective role of catalase in *Pseudomonas aeruginosa* biofilm resistance to hydrogen
301 peroxide. *Appl. Environ. Microbiol.* 65, 4594–4600.
- 302 Peralta, E., Natividad, R., Roa, G., Marin, R., Romero, R., Pavon, T., 2013. A
303 comparative study on the electrochemical production of H₂O₂ between BDD and graphite
304 cathodes. *Sustain. Environ. Res.* 23, 259–266.
- 305 Pliuta, V.A., Andreenko, I.V., Kuznetsov, A.E., Khmel', I.A., 2013. [Formation of the
306 *Pseudomonas aeruginosa* PAO1 biofilms in the presence of hydrogen peroxide; the effect
307 of the AiiA gene]. *Mol. Genet. Mikrobiol. Virusol.* 10–14.
- 308 Qiang, Z., Chang, J.-H., Huang, C.-P., 2002. Electrochemical generation of hydrogen
309 peroxide from dissolved oxygen in acidic solutions. *Water Res.* 36, 85–94.
310 doi:10.1016/S0043-1354(01)00235-4
- 311 Stewart, P.S., Roe, F., Rayner, J., Elkins, J.G., Lewandowski, Z., Ochsner, U.A., Hassett,
312 D.J., 2000. Effect of Catalase on Hydrogen Peroxide Penetration into *Pseudomonas*
313 *aeruginosa* Biofilms. *Appl. Environ. Microbiol.* 66, 836–838.
- 314 Jiao, Y., Zheng, Y., Jaroniec, M., Qiao, S.Z., 2015. Design of electrocatalysts for oxygen-
315 and hydrogen-involving energy conversion reactions. *Chem. Soc. Rev.* 44, 2060–2086.
316 doi:10.1039/c4cs00470a
- 317 Ramaswamy, N., Mukerjee, S., 2012. Fundamental Mechanistic Understanding of
318 Electrocatalysis of Oxygen Reduction on Pt and Non-Pt Surfaces: Acid versus Alkaline
319 Media [WWW Document]. *Adv. Phys. Chem.* doi:10.1155/2012/491604
- 320 Sánchez-Sánchez, C.M., Bard, A.J., 2009. Hydrogen Peroxide Production in the Oxygen
321 Reduction Reaction at Different Electrocatalysts as Quantified by Scanning
322 Electrochemical Microscopy. *Anal. Chem.* 81, 8094–8100. doi:10.1021/ac901291v
- 323
- 324