

Supporting Information for

Efficient Conversion of Light Cycle Oil into High Octane Number Gasoline and Light Olefins over Mesoporous ZSM-5 catalyst

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Table S1. Properties of the LCO

properties	LCO
distillation (ASTM D2887)	
10/50/90 % (°C)	273/304/321
density at 15 °C (kg/m ³)	945
carbon residue (wt.%)	0.37
condensation point (°C)	27
viscosity at 15 °C (mm ² ·s ⁻¹)	9.89
flash point (°C)	82
cetane index	17.1
(CI, ASTM D4737-04)	

Table S2. Properties of the Hydrogenation Catalyst

property	value
shape	trefoil bar
diameter (mm)	1.51-1.53
length (mm)	2-4
chemical composition (wt.%)	
MoO ₃	20.0-23.0
NiO	2.0-3.0
pore volume (cm ³ /g)	0.33-0.36
surface area (m ² /g)	200-240
packing density (kg/m ³)	810-820

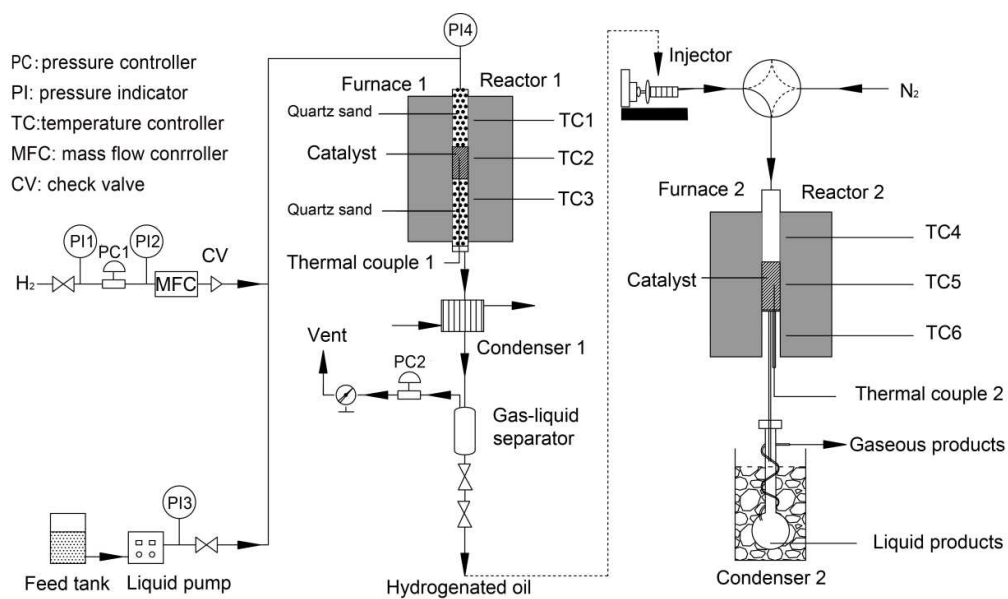


Figure S1. Diagram of the experimental process.

**Table S3. Ratio of light alkanes and light olefins in LPG of hydro-LCO
conversion over the meso-ZSM-5 and ZSM-5 catalyst**

catalyst	520 °C	540 °C	560 °C	580 °C
meso-ZSM-5	0.38	0.34	0.31	0.28
ZSM-5	0.34	0.33	0.37	0.39

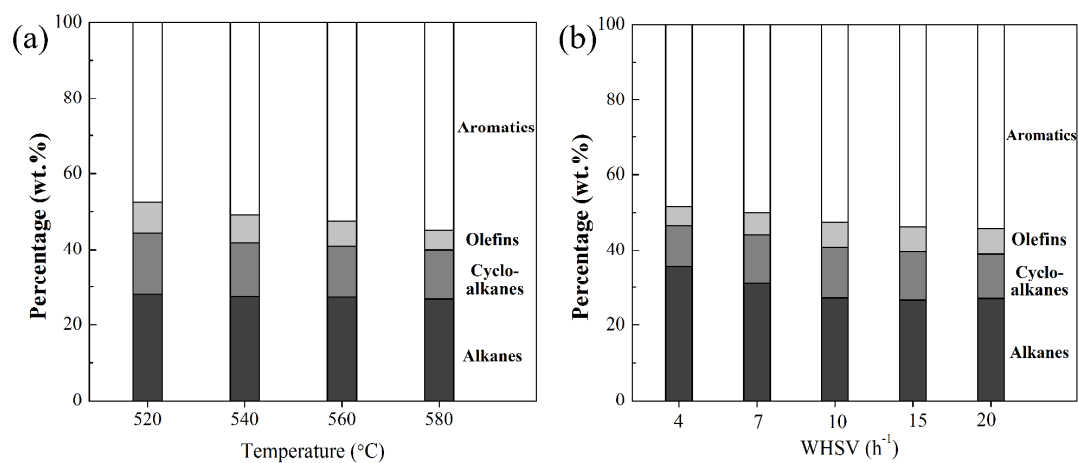
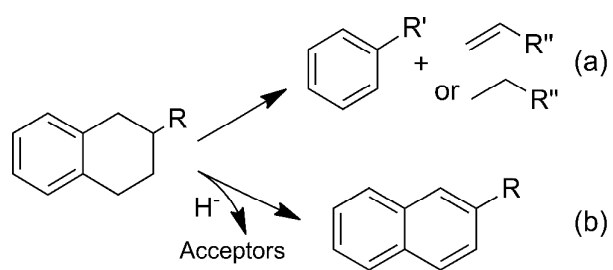


Figure S2. Compositions of gasoline of hydro-LCO conversion over the meso-ZSM-5 catalyst as a function of reaction temperature (a), and WHSV (b).



Scheme S1. Reaction pathways of tetralins in catalytic cracking process.

Definition of tetralins conversion and its ring opening selectivity:

$$\text{Tetralins conversion (wt.\%)} = 100 - \frac{\text{Mass of tetralins in unconverted hydro-LCO}}{\text{Mass of tetralins in hydro-LCO feed}} \times 100$$

$$\text{Tetralins ring opening selectivity (wt.\%)} = 100 - \frac{\text{Mass of PAHs formed}}{\text{Mass of converted tetralins}} \times 100$$

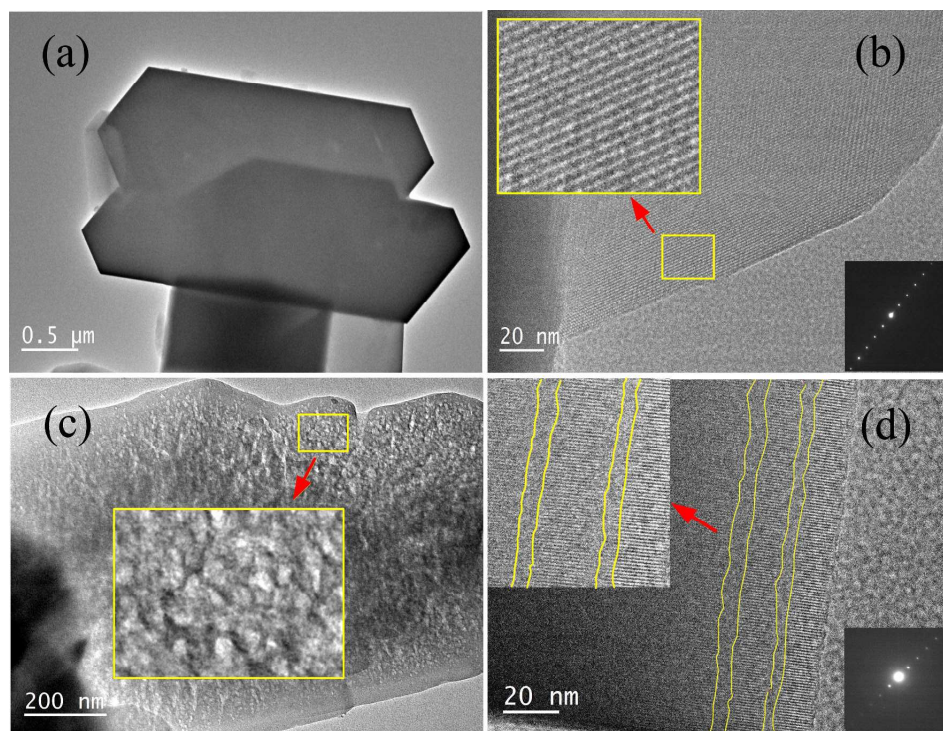


Figure S3. TEM images of parent ZSM-5 (a) and (b), and meso-ZSM-5 (c) and (d) zeolites; (b) and (d) with electron diffraction patterns.

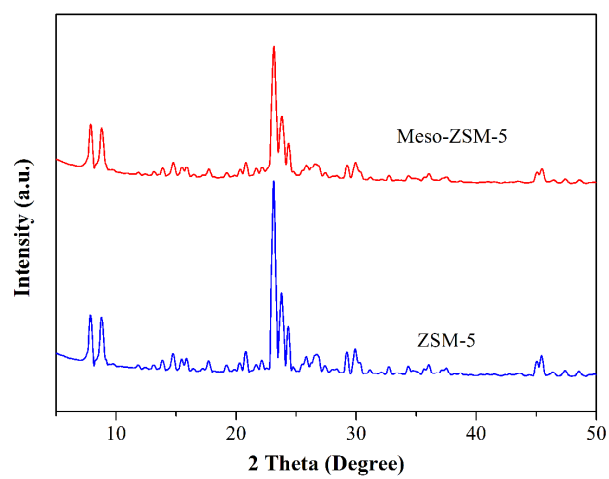


Figure S4. XRD patterns of the parent ZSM-5 and meso-ZSM-5 zeolites.

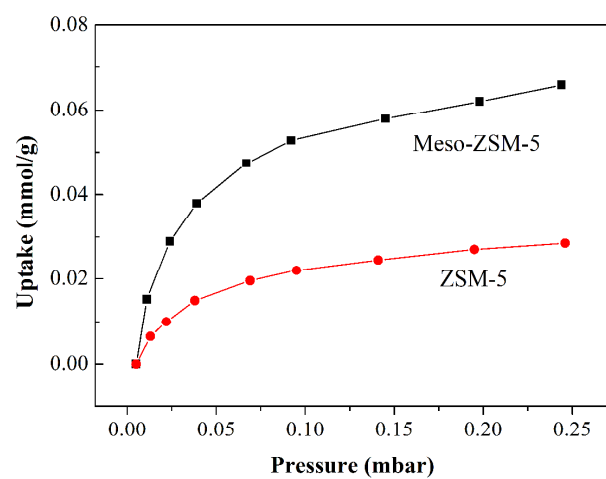


Figure S5. Adsorption isotherms of tetralin at 298 K by IGA on ZSM-5 and meso-ZSM-5 zeolites.