

**Kinetic and Mechanism of the Cleavage of Phthalic Anhydride in Glacial Acetic Acid
Solvent Containing Aniline**

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Supporting Informations

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TABLE I. Effects of Mixed H₂O – CS Solvents on Absorbance (A_{ob}) of 1.0 x 10⁻³ M Ani at 275 nm, 0.1 M NaOH and 0.1, 1.0 M HCl at 35 °C

CS ^a % v/v	A _{ob} ^b	A _{ob} ^c	CS ^d	A _{ob} ^b	A _{ob} ^c	A _{ob} ^e	ΔA _{ob} ^f	ΔA _{ob} ^g % v/v
1	1.232	0.002	1	1.177	0.005	0.012	- 0.007	0.0
10	1.223	0.008	10	1.198	0.014	0.014	0.004	0.004
20	1.209	0.007	20	1.203	0.025	0.015	0.008	- 0.002
30	1.194	0.005	30	1.182	0.035	0.026	0.018	0.009
40	1.168	0.005	40	1.144	0.044	0.025	0.026	0.007
50	1.158	0.010	50	1.128	0.052	0.029	0.032	0.009
60	1.129	0.012	60	h	0.063	0.030	0.039	0.006
70	h	0.006	70	h	0.081	0.033	0.053	0.005
80	h	0.010	80	h	0.083	0.037	0.061	0.005
90	h	0.010	90	h	0.093	0.054	0.053	0.014

^a CS = CH₃CN. ^b Each mixed aqueous solution contained 0.1 M NaOH. ^c Each mixed aqueous solution contained 0.1 M HCl. ^d CS = THF. ^e Each mixed aqueous solution contained 1.0 M HCl.

^f ΔA_{ob} = A_{ob} (at 0.1 M HCl) – A_{ob} (at 0.0 M HCl). ^g ΔA_{ob} = A_{ob} (at 1.0 M HCl) – A_{ob} (at 0.0 M HCl). ^h Precipitation occurred in the solution.

TABLE II. Values of α^∞ and δ_{ob}^∞ , Calculated from Eq 3 (with $\alpha = \alpha^\infty$, $\delta_{ob} = \delta_{ob}^\infty$) Using A_∞^a

AcOH	CS ^b	$10^2 \alpha^\infty$	δ_{ob}^∞	N ^c	T ^e	[Ani] _T ^d range
% v/v	%v/v		M ⁻¹ cm ⁻¹		°C	M
100	0	85.3 ± 3.1^e	208 ± 12^e	5	30	1.0×10^{-3} - 4.0×10^{-3}
100	0	98.4 ± 6.7	168 ± 27	5	30	1.0×10^{-3} - 4.0×10^{-3}
100	0	98.2 ± 5.3	253 ± 21	5	35	1.0×10^{-3} - 4.0×10^{-3}
100	0	89.4 ± 3.3	240 ± 13	5	35	1.0×10^{-3} - 4.0×10^{-3}
100	0	83.1 ± 2.1	258 ± 8	5	40	1.0×10^{-3} - 4.0×10^{-3}
100	0	81.9 ± 6.8	276 ± 27	5	40	1.0×10^{-3} - 4.0×10^{-3}
100	0	80.1 ± 3.0	298 ± 11	5	45	1.0×10^{-3} - 4.0×10^{-3}
100	0	74.6 ± 6.1	345 ± 31	4	50	1.0×10^{-3} - 3.0×10^{-3}
99	1 ^f	60.5 ± 1.2	205 ± 5	8	35	1.0×10^{-3} - 4.0×10^{-3}
95	5 ^f	61.6 ± 1.5	223 ± 7	8	35	1.0×10^{-3} - 4.0×10^{-3}
90	10 ^f	61.0 ± 4.5	230 ± 20	8	35	1.0×10^{-3} - 4.0×10^{-3}
85	15 ^f	58.3 ± 1.6	271 ± 7	8	35	1.0×10^{-3} - 4.0×10^{-3}
80	20 ^f	58.0 ± 1.9	277 ± 8	8	35	1.0×10^{-3} - 4.0×10^{-3}
75	25 ^f	56.6 ± 2.1	305 ± 9	8	35	1.0×10^{-3} - 4.0×10^{-3}
70	30 ^f	55.3 ± 1.8	315 ± 8	8	35	1.0×10^{-3} - 4.0×10^{-3}
60	40 ^f	47.1 ± 1.6	406 ± 8	7	35	1.0×10^{-3} - 4.0×10^{-3}
50	50 ^f	43.0 ± 1.2	506 ± 6	7	35	1.0×10^{-3} - 3.0×10^{-3}
40	60 ^f	41.6 ± 0.4	629 ± 2	6	35	1.0×10^{-3} - 2.5×10^{-3}
30	70 ^f	41.9 ± 1.2	771 ± 10	9	35	4.0×10^{-4} - 2.0×10^{-3}
20	80 ^f	39.6 ± 1.9	994 ± 19	6	35	4.0×10^{-4} - 1.5×10^{-3}
10	90 ^f	53.4 ± 0.5	1035 ± 5	5	35	3.5×10^{-4} - 1.3×10^{-3}
95	5 ^g	62.5 ± 1.6	266 ± 7	8	35	1.0×10^{-3} - 4.0×10^{-3}
90	10 ^g	70.2 ± 2.3	274 ± 10	8	35	1.0×10^{-3} - 4.0×10^{-3}
85	15 ^g	66.1 ± 3.3	352 ± 17	8	35	8.0×10^{-4} - 3.0×10^{-4}
80	20 ^g	67.2 ± 1.2	411 ± 7	7	35	1.0×10^{-3} - 4.0×10^{-3}

75	25 ^g	66.2 ± 0.8	505 ± 5	7	35	$8.0 \times 10^{-4} - 2.5 \times 10^{-3}$
70	30 ^g	68.1 ± 1.2	571 ± 8	6	35	$8.0 \times 10^{-4} - 2.0 \times 10^{-3}$
60	40 ^g	63.7 ± 0.9	789 ± 9	6	35	$4.0 \times 10^{-4} - 1.5 \times 10^{-3}$
50	50 ^g	62.6 ± 1.6	937 ± 20	6	35	$4.0 \times 10^{-4} - 1.3 \times 10^{-3}$
40	60 ^g	66.2 ± 1.1	991 ± 14	6	35	$4.0 \times 10^{-4} - 1.3 \times 10^{-3}$
40	60 ^g	62.5 ± 1.1	1021 ± 14	6	35	$3.0 \times 10^{-4} - 1.3 \times 10^{-3}$
35	65 ^g	61.5 ± 1.3	1083 ± 20	6	35	$3.0 \times 10^{-4} - 1.0 \times 10^{-3}$
30	70 ^g	67.3 ± 1.8	1072 ± 27	5	35	$4.0 \times 10^{-4} - 1.0 \times 10^{-3}$
30	70 ^g	64.1 ± 1.8	1073 ± 28	6	35	$3.0 \times 10^{-4} - 1.0 \times 10^{-3}$
25	75 ^g	66.6 ± 2.4	1159 ± 37	6	35	$3.0 \times 10^{-4} - 1.0 \times 10^{-3}$
20	80 ^g	67.8 ± 3.2	1086 ± 46	5	35	$4.0 \times 10^{-4} - 1.0 \times 10^{-3}$
20	80 ^g	70.0 ± 1.1	1071 ± 17	6	35	$3.0 \times 10^{-4} - 1.0 \times 10^{-3}$
15	85 ^g	69.9 ± 1.3	1084 ± 20	6	35	$3.0 \times 10^{-4} - 1.0 \times 10^{-3}$
10	90 ^g	72.5 ± 2.4	997 ± 35	5	35	$4.0 \times 10^{-4} - 1.0 \times 10^{-3}$
10	90 ^g	70.6 ± 1.8	1068 ± 28	6	35	$3.0 \times 10^{-4} - 1.0 \times 10^{-3}$

^a $[PAn_0] = 1.5 \times 10^{-4}$ M, T = 35 °C. ^b CS = Co-solvent. ^c Total number of kinetic runs. ^d Total concentration range of aniline. ^e Error limits are standard deviations. ^f CS = CH₃CN ^g CS = THF.

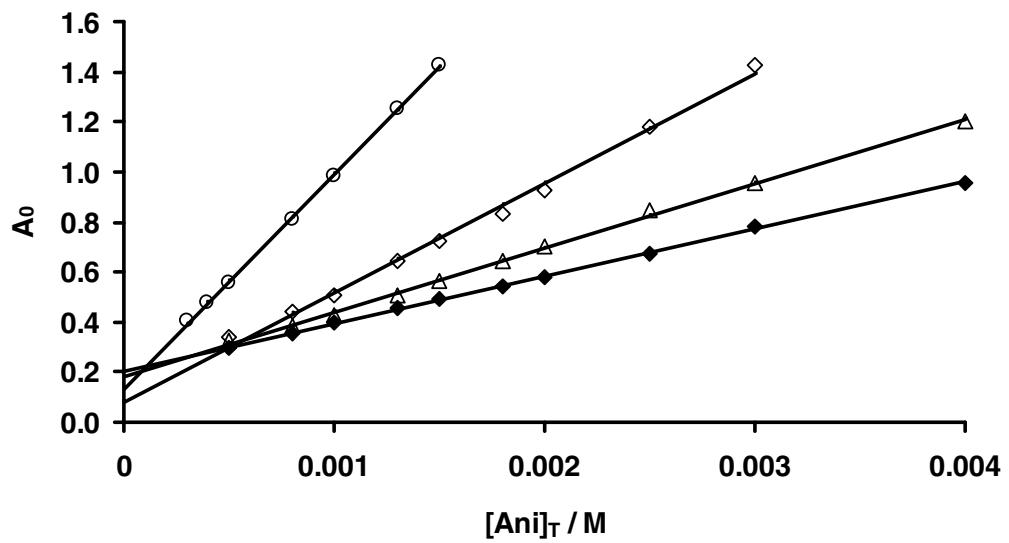


Figure I a. Plots showing the dependence of A_0 versus $[Ani]_T$ at 5% (\blacklozenge), 25% (\triangle), 50% (\diamond) and 80% (\circ) v/v CH_3CN in mixed CH_3CN -AcOH solvents. The solid lines are drawn through the calculated data points using eq 3, and the parameters, α and δ_{ob} , listed in Table 2.

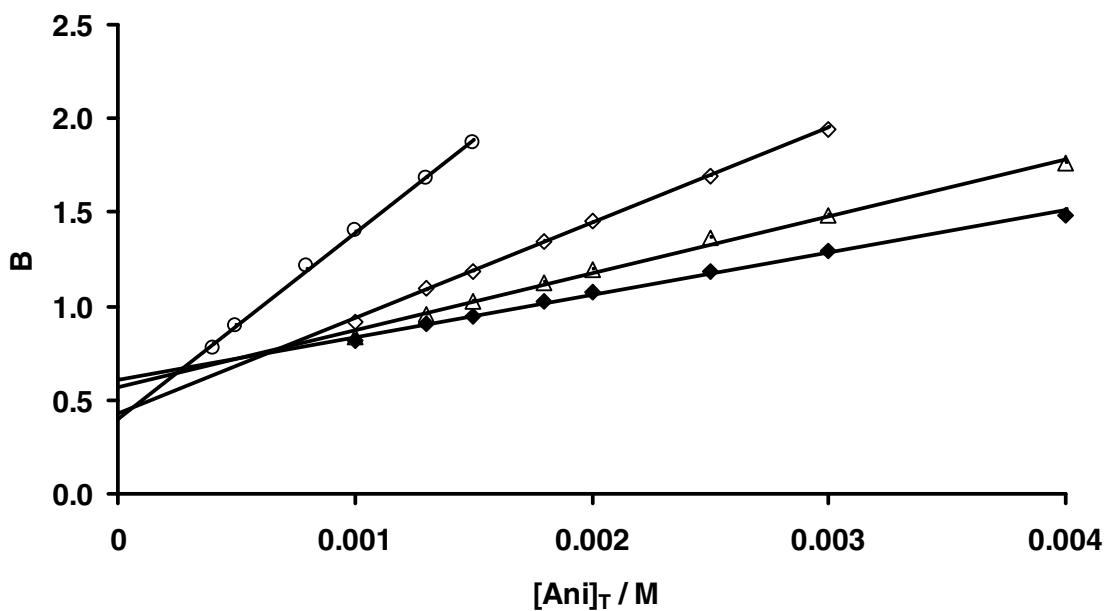


Figure I b. Plots showing the dependence of B ($= A_\infty$) versus $[Ani]_T$ at 5% (\blacklozenge), 25% (Δ) , 50% (\diamond) and 80% (\circ) v/v CH_3CN in mixed CH_3CN -AcOH solvents. The solid lines are drawn through the calculated data points using eq 3 (with $A_0 = A_\infty$, $\alpha = \alpha^\infty$ and $\delta_{ob} = \delta_{ob}^\infty$) the parameters, α^∞ and δ_{ob}^∞ , listed in Table II (SI).

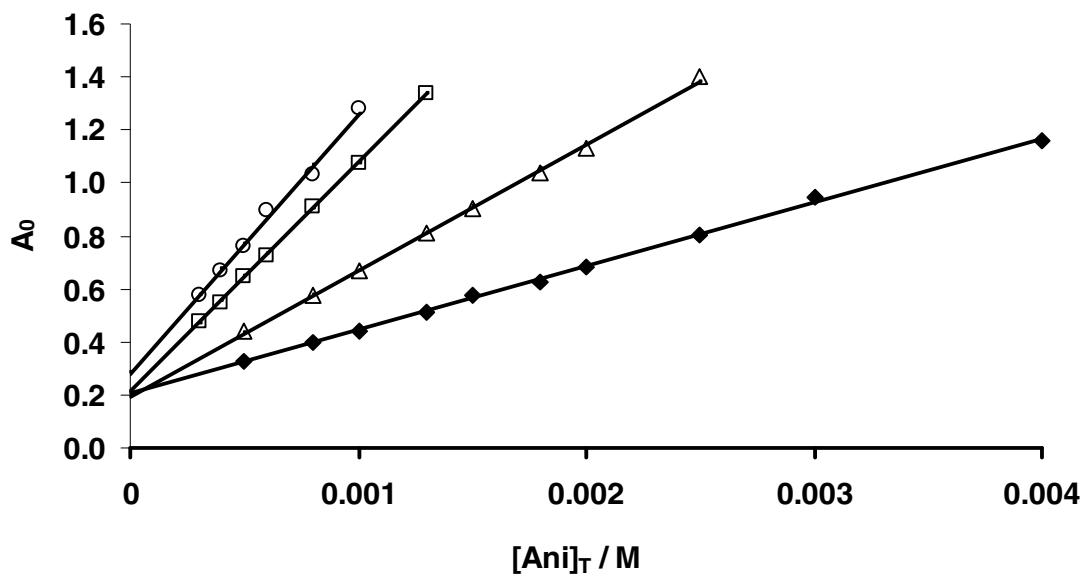


Figure II a. Plots showing the dependence of A_0 versus $[Ani]_T$ at 5% (\blacklozenge), 25% (\triangle), 50% (\square) and 85% (\circ) v/v THF in mixed THF-AcOH solvents. The solid lines are drawn through the calculated data points using eq 3 and the parameters, α and δ_{ob} , listed in Table 2.

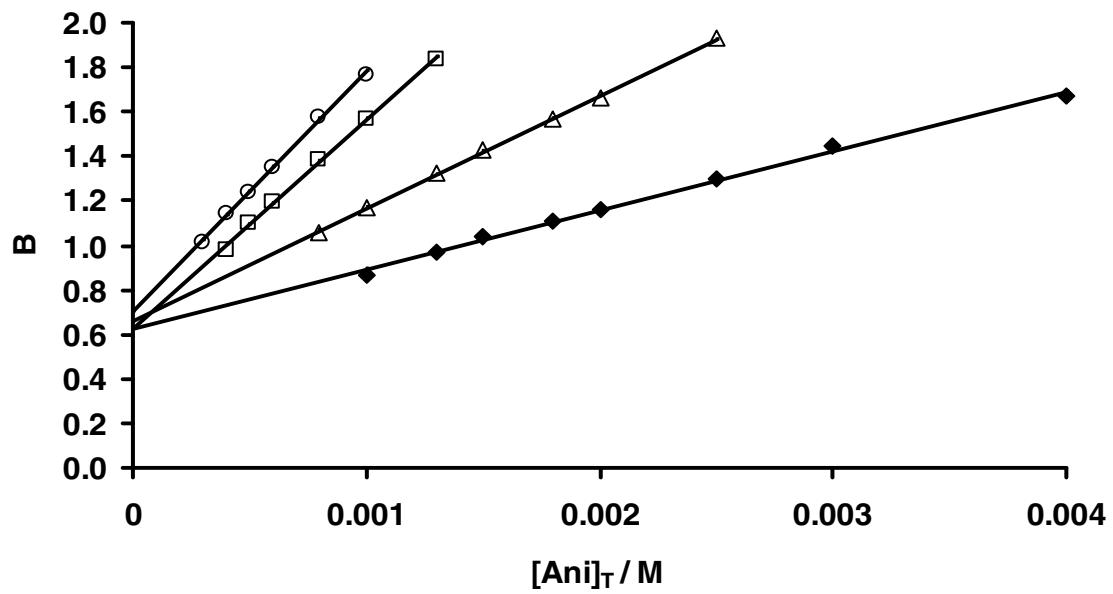


Figure II b. Plots showing the dependence of B ($= A_\infty$) versus $[Ani]_T$ at 5% (\blacklozenge), 25% (Δ), 50% (\square) and 85% (\circ) v/v THF in mixed THF-AcOH solvents. The solid lines are drawn through the calculated data points using eq 3 (with $A_0 = A_\infty$, $\alpha = \alpha^\infty$ and $\delta_{ob} = \delta_{ob}^\infty$) and the parameters, α^∞ and δ_{ob}^∞ , listed in Table II (SI).