

## ***Supporting Information***

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### **Fabrication of Pd/In<sub>2</sub>O<sub>3</sub> Nanocatalysts Derived from MIL-68(In) Loaded with Molecular Metalloporphyrin (TCPP(Pd)) Towards CO<sub>2</sub> Hydrogenation to Methanol**

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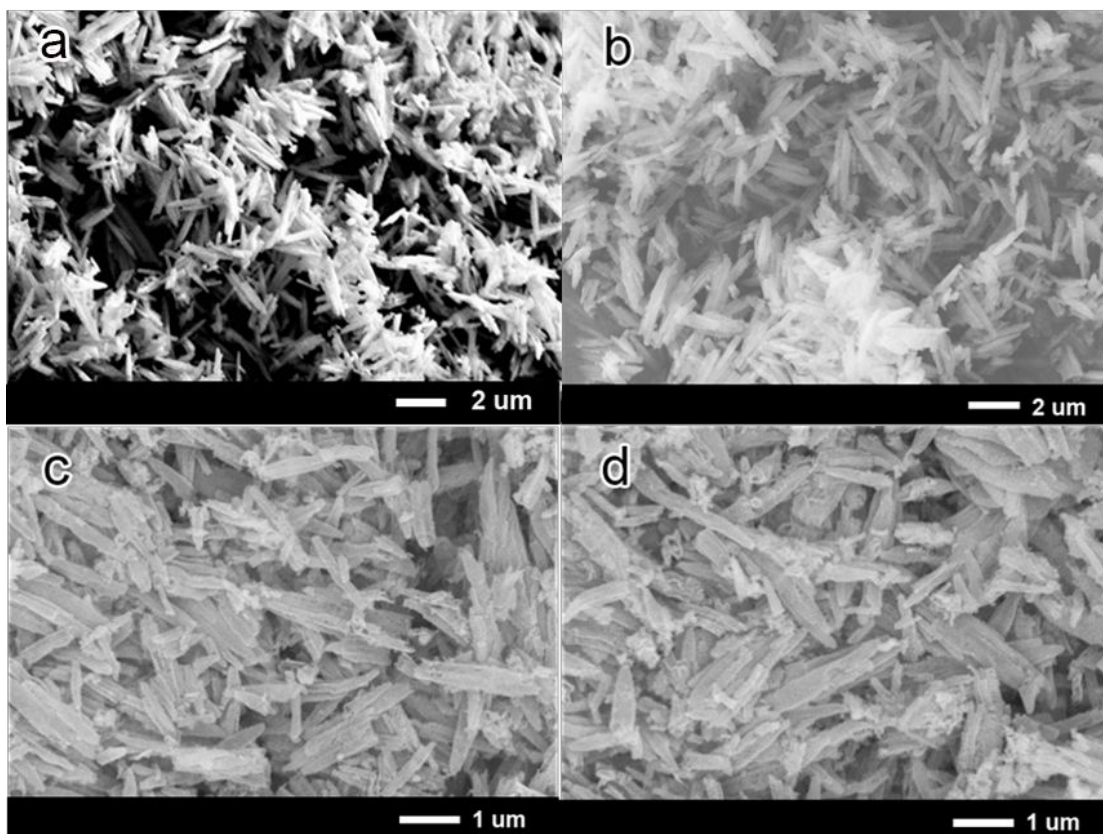
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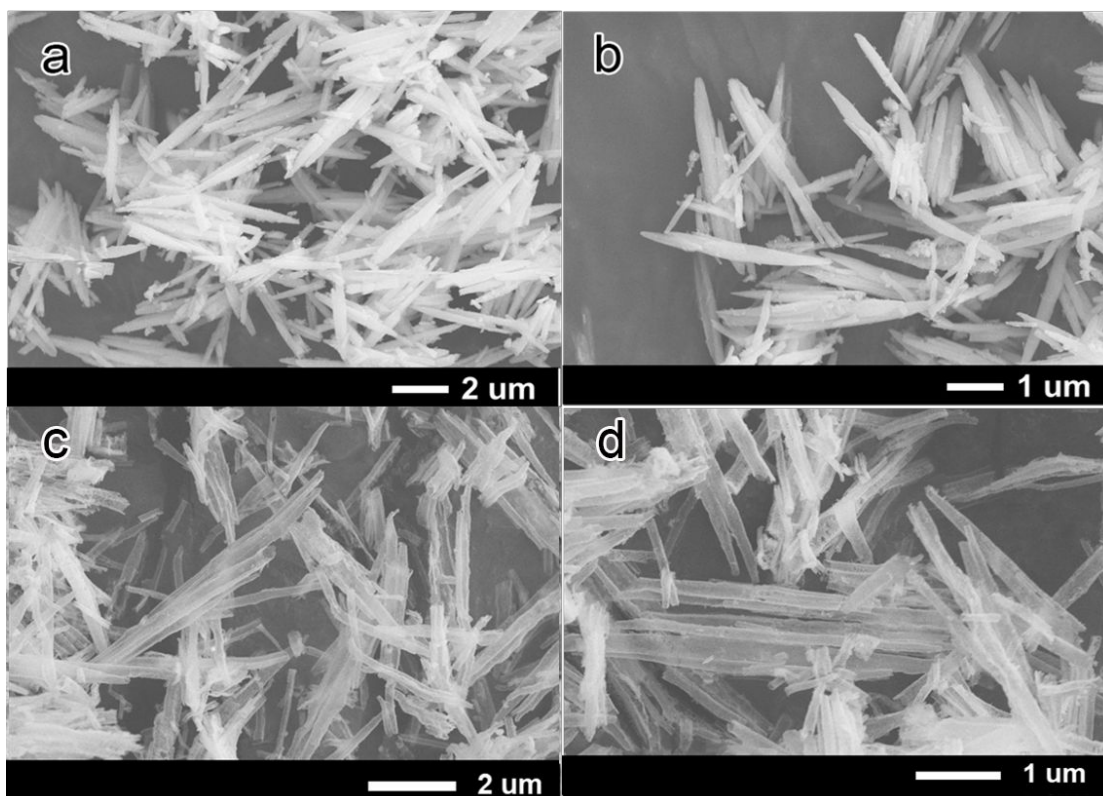
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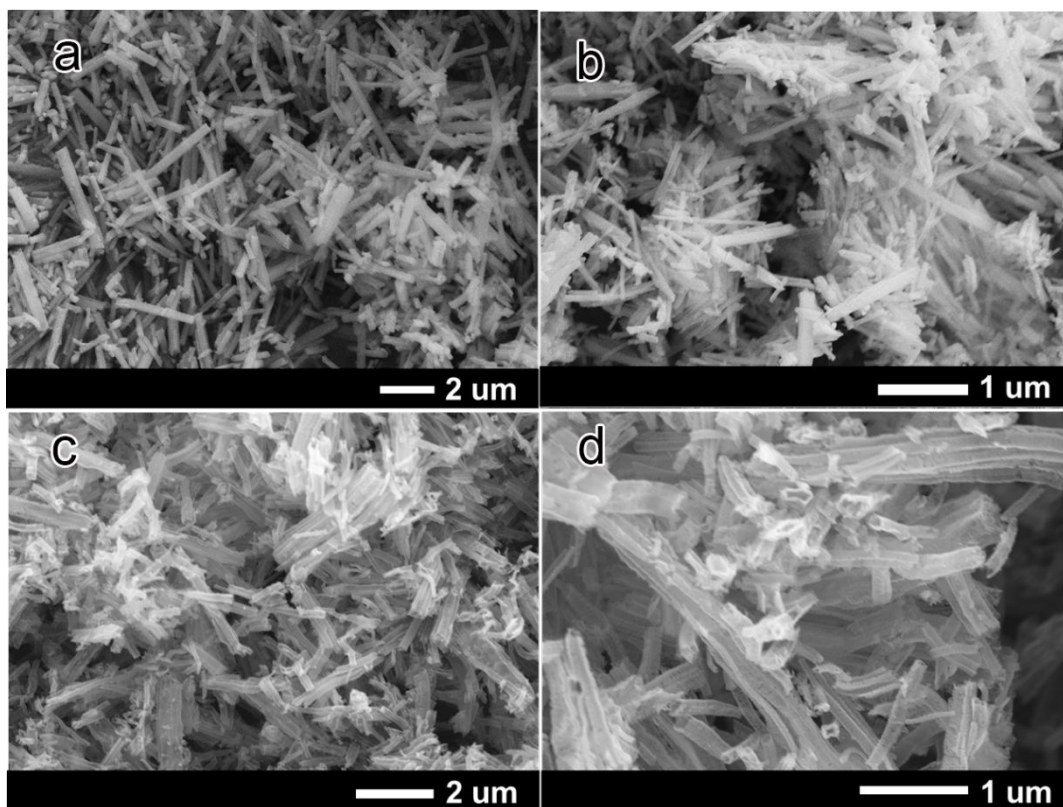
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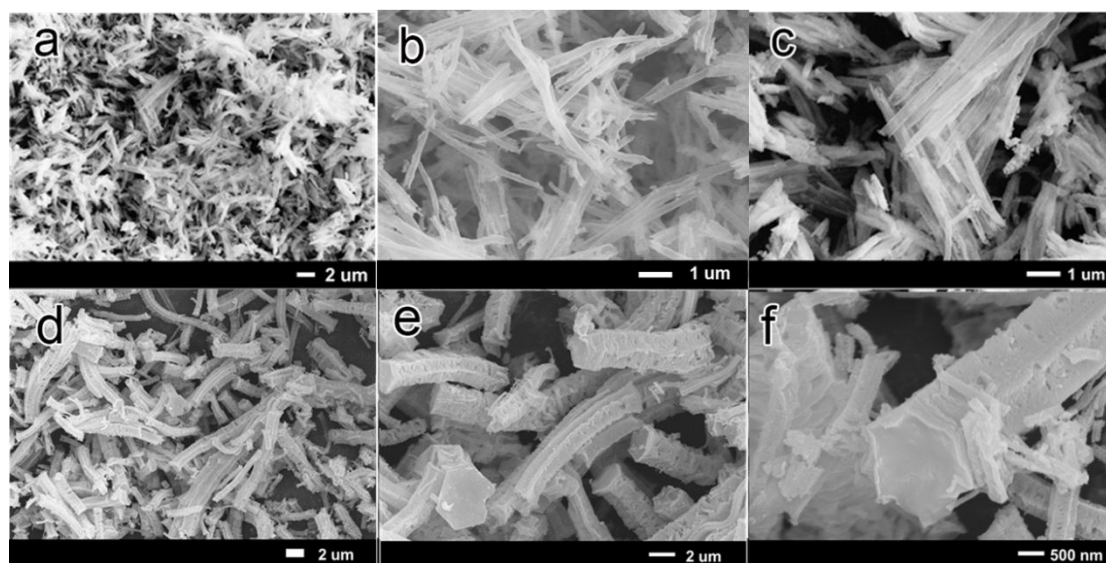
**Figure S1.** Representative SEM images of TCPP(Pd)@MIL-68(In) at TCPP(Pd) loading content of 1.9 wt% (a-b), and (c-d) derived Pd@In<sub>2</sub>O<sub>3</sub> catalyst.



**Figure S2.** Representative SEM images of TCPP(Pd)@MIL-68(In) at TCPP(Pd) loading content of 3.8 wt% (a-b), and (c-d) derived Pd@In<sub>2</sub>O<sub>3</sub> catalyst.

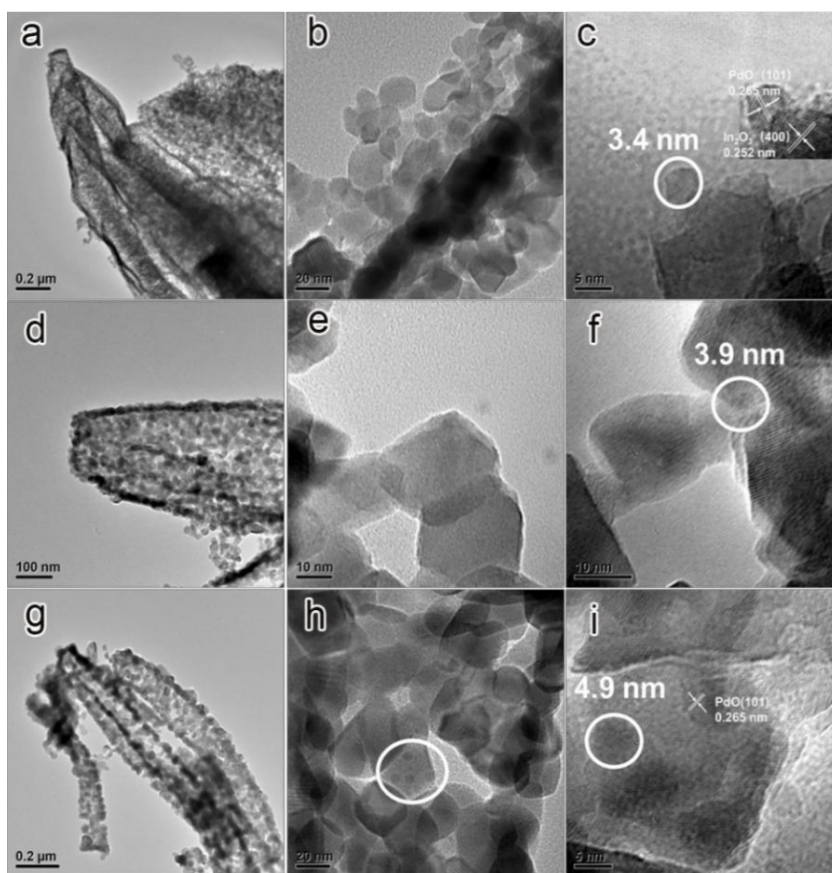


**Figure S3.** Representative SEM images of TCPP(Pd)@MIL-68(In) at TCPP(Pd) loading content of 4.7 wt% (a-b), and (c-d) the derived Pd@In<sub>2</sub>O<sub>3</sub> catalyst.

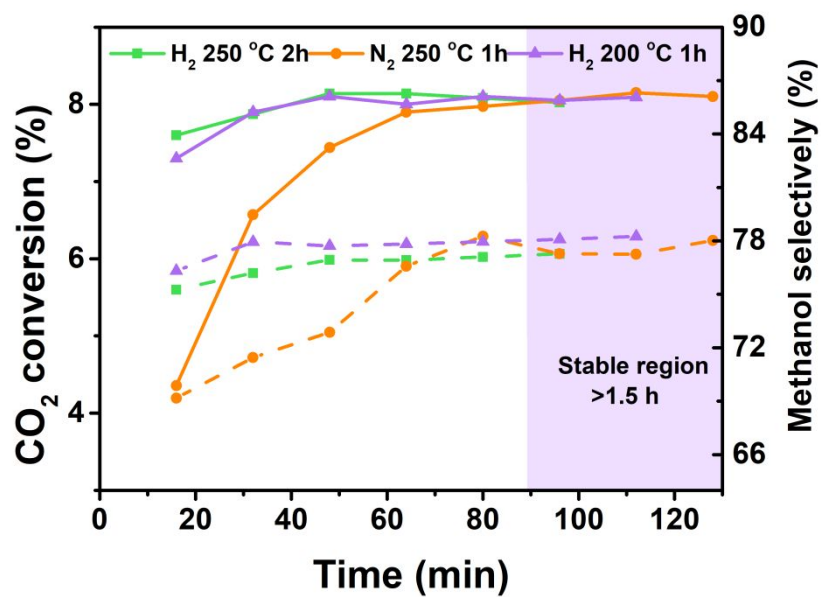


**Figure S4.** Representative SEM images of (a) Pd@In<sub>2</sub>O<sub>3</sub> catalyst derived from Pd-TCPP@MIL-68(In) at TCPP(Pd) loading content of 2.8 wt%, (d-f) IWI-Pd-In<sub>2</sub>O<sub>3</sub> catalyst prepared from using Pd<sup>2+</sup>@MIL-68(In) as a precursor.





**Figure S5.** Representative TEM images at different magnifications of Pd@In<sub>2</sub>O<sub>3-x</sub> catalysts with different calcination temperatures. (a-c) 600 °C, (d-f) 700 °C, and (g-i) 800 °C.



**Figure S6.** The comparisons of CO<sub>2</sub> conversion and methanol selectivity over the Pd@In<sub>2</sub>O<sub>3</sub> catalyst under different pretreatment conditions (temperature, time, and atmospheres).

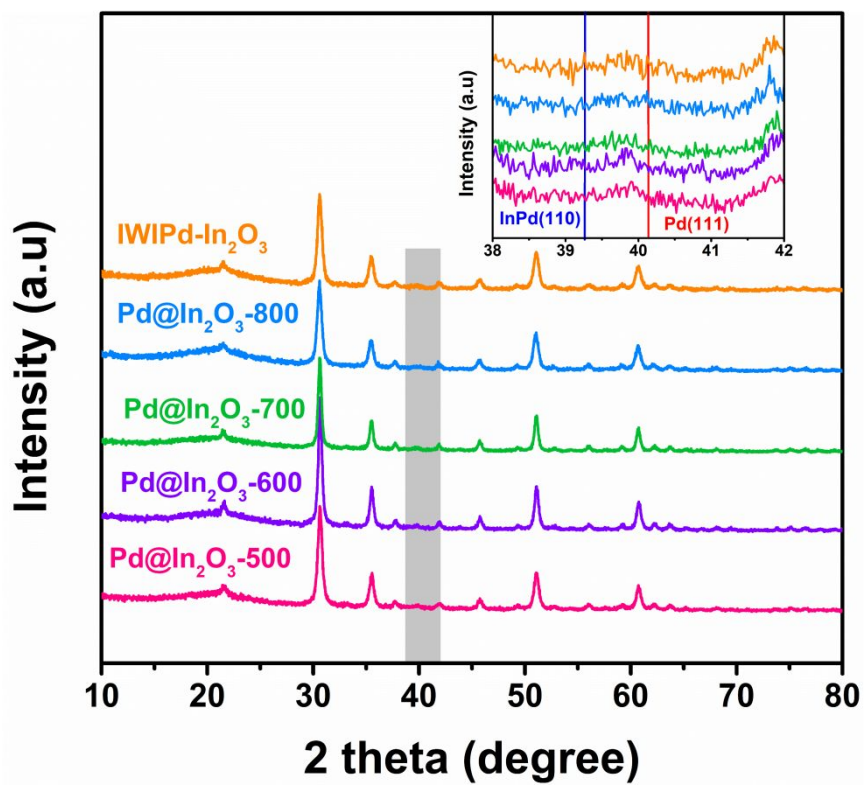
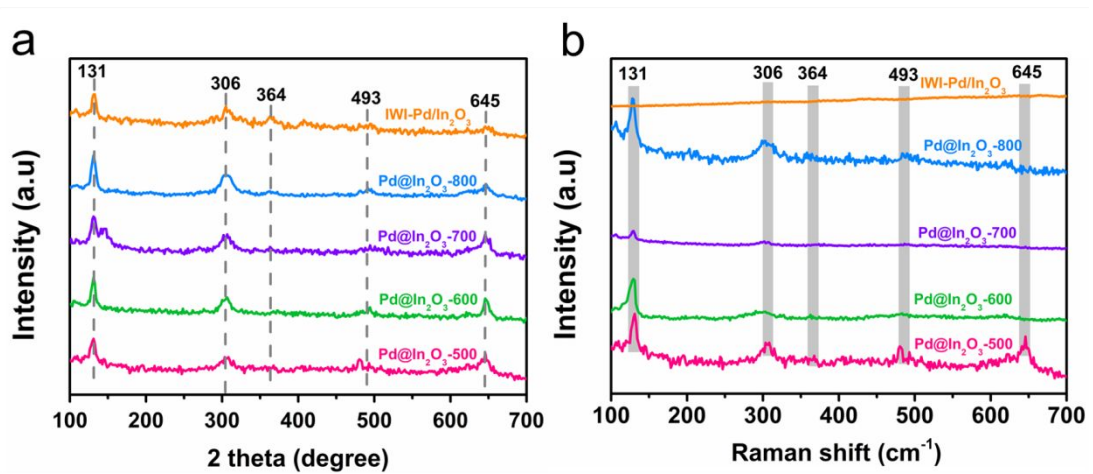
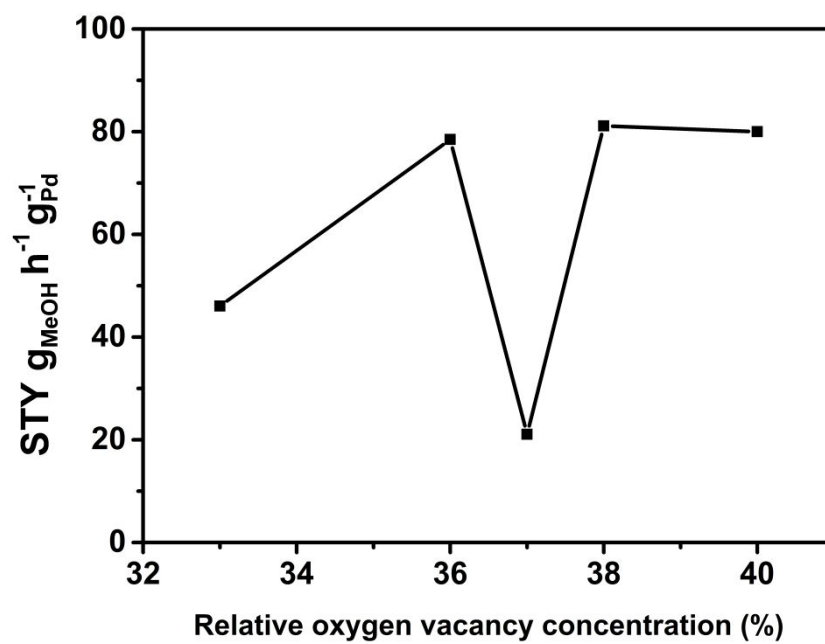


Figure S7. XRD patterns of the spent Pd/In<sub>2</sub>O<sub>3</sub> and IWI-Pd/In<sub>2</sub>O<sub>3</sub> catalysts.

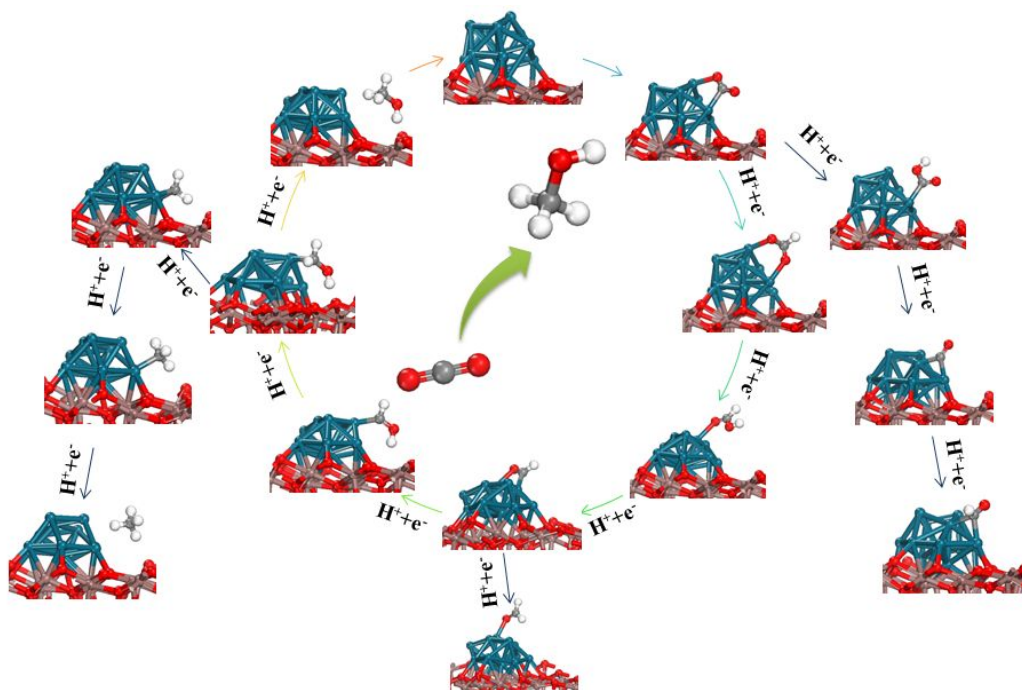




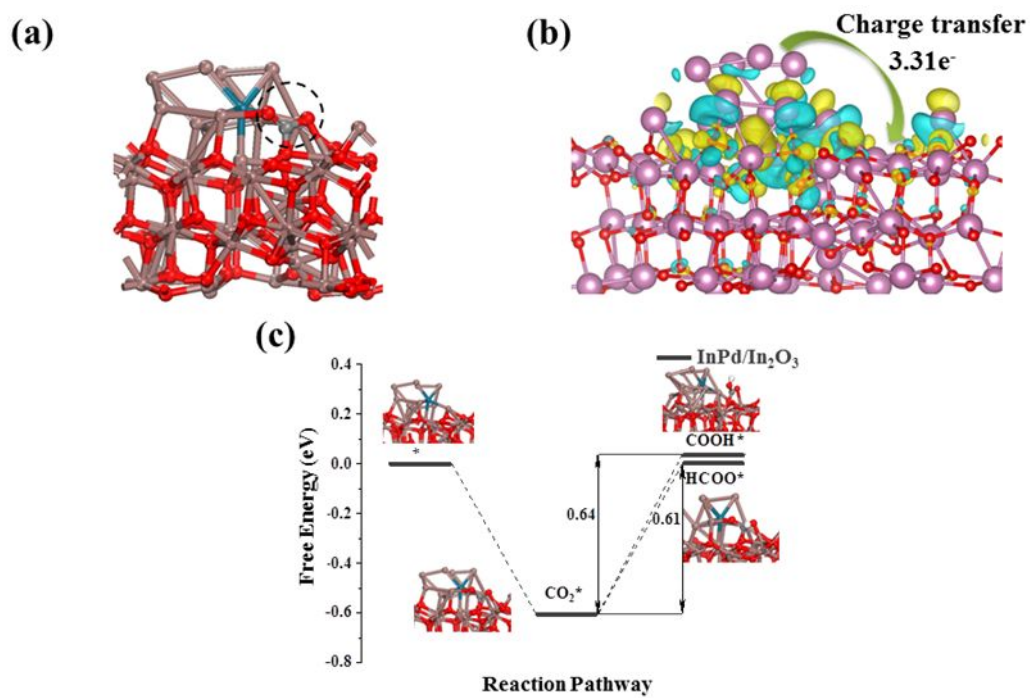
**Figure S8.** (a) Raman spectra of the calcination catalyst and (b) Raman spectra of the spent catalyst.



**Figure S9.** The space-time yield (STY) of methanol as a function of the relative concentration of oxygen vacancy.



**Figure S10.** Structure diagrams of the important intermediates in the catalytic CO<sub>2</sub> hydrogenation on the surface of the Pd/In<sub>2</sub>O<sub>3</sub> catalyst. Color codes: white, H atoms; red, O atoms; brown, In atoms; cyan, Pd atoms.



**Figure S11.** (a) CO<sub>2</sub> adsorption structure, (b) charge transfer, and (c) the catalytic pathway on the InPd/In<sub>2</sub>O<sub>3</sub> catalyst.

**Table S1** Synthetic parameters and the corresponding average length and width of the prepared MIL-68(In) composites.

Sample	TCPD(Pd) (mg)	H <sub>2</sub> BDC (mg)	In(NO <sub>3</sub> ) <sub>3</sub> (mg)	DMF (mL)	Length ( $\mu$ m)	Width ( $\mu$ m)	S <sub>BET</sub> m <sup>2</sup> /g	V <sub>pore</sub> cm <sup>3</sup> / g
TCPD(Pd) @MIL- 68(In)	0	200	408.2	5.0	4.6 $\pm$ 0.5	1.0 $\pm$ 0.2	846	0.68
	10	200	408.2	5.0	6.0 $\pm$ 1.2	1.0 $\pm$ 0.2	701.5	0.46
	15	200	408.2	5.0	6.9 $\pm$ 1.0	1.4 $\pm$ 0.2	675.9	0.20
	20	200	408.2	5.0	8.1 $\pm$ 1.5	1.4 $\pm$ 0.5	156.6	0.11
	25	200	408.2	5.0	8.4 $\pm$ 1.5	1.4 $\pm$ 0.4	60.5	0.08
	30	200	408.2	5.0	8.5 $\pm$ 1.5	1.4 $\pm$ 0.6	n.a.	n.a.

**Table S2** Comparison of CO<sub>2</sub> hydrogenation to methanol over different catalysts.

Catalyst	T [K]	P [MPa]	GHSV (mL g <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup> )	S <sub>MeOH</sub> (%)	STY <sub>MeOH</sub> (g <sub>MeOH</sub> h <sup>-1</sup> g <sub>x</sub> <sup>-1</sup> )	Ref.
PdIn-In <sub>2</sub> O <sub>3</sub> /SiO <sub>2</sub> <sup>a</sup>	573	5.0	63000	24	3.6	1
Pd/In <sub>2</sub> O <sub>3</sub> -CP <sup>b</sup>	553	5.0	24000	75	81.3	2
Pd/In <sub>2</sub> O <sub>3</sub> /SBA-15	543	5.0	15000	83.9	3.5	3
Pd-P/In <sub>2</sub> O <sub>3</sub> <sup>c</sup>	573	5.0	21000	71	97.8	4
Pt/In <sub>2</sub> O <sub>3</sub>	573	5.0	21000	54	52.6	5
Au/In <sub>2</sub> O <sub>3</sub>	573	5.0	21000	67.8	23.2	6
Ir/In <sub>2</sub> O <sub>3</sub>	573	5.0	21000	70	7.65	7
Pd/CeO <sub>2</sub>	513	3.0	6000	47.7	1.16	8
Pd-ZnO@ZIF-8	563	4.5	19200	78	19.8	9
<i>h</i> -In <sub>2</sub> O <sub>3</sub> /Pd <sup>d</sup>	568	3.0	24000	74	41.9	10
Pd@In <sub>2</sub> O <sub>3</sub> -500	568	3.0	19200	74	79.2	our work
Pd@In <sub>2</sub> O <sub>3</sub> -600	568	3.0	19200	81	81.1	our work

Notes: S<sub>MeOH</sub> represents the selectivity of methanol, and STY<sub>MeOH</sub> represents the space-time yield of methanol-based on the weight of the supported noble metals such as Pd, Pt, Au, and Ir, etc.

<sup>a</sup>: Both PdIn alloy and In<sub>2</sub>O<sub>3</sub> were supported on SiO<sub>2</sub>.

<sup>b</sup>: Pd-In<sub>2</sub>O<sub>3</sub> catalyst was synthesized by co-precipitated (CP).

<sup>c</sup>: Pd was supported on In<sub>2</sub>O<sub>3</sub> by using the peptide as a modifier (Pd-P).

<sup>d</sup>: Pd nanoparticles were supported on hollow-tube structure In<sub>2</sub>O<sub>3</sub> (*h*-In<sub>2</sub>O<sub>3</sub>).



**Table S3** Comparison of the M/In<sub>2</sub>O<sub>3</sub> catalysts with different noble metals loading contents on In<sub>2</sub>O<sub>3</sub> support for CO<sub>2</sub> hydrogenation.

Catalyst	Noble metal loading (wt%)	Temp. (K)	Pressure (MPa)	H <sub>2</sub> /CO <sub>2</sub>	Catalytic performance		Ref.
					CO <sub>2</sub> conv. (%)	Methanol selec. (%)	
Pd/In <sub>2</sub> O <sub>3</sub>	0.93	573	5.0	4	20	71	4
Pd/In <sub>2</sub> O <sub>3</sub>	0.75	553	5.0	4	9.2	78	2
Pd/In <sub>2</sub> O <sub>3</sub>	1.36	568	3.0	3	10.5	72.4	10
Pd/In <sub>2</sub> O <sub>3</sub>	5.0	523	3.	3	1.9	72	10
Pt/In <sub>2</sub> O <sub>3</sub>	1.07	573	5.0	4	17.3	54	10
Au/In <sub>2</sub> O <sub>3</sub>	2.0	573	5.0	4	11.7	67.8	10
Ir/In <sub>2</sub> O <sub>3</sub>	1.0	573	5.0	4	11.6	70	10
Pd@In <sub>2</sub> O <sub>3</sub>	0.5	568	3.0	3	8.1	81.1	our work

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